

## Article

# Inspection-Oriented Predictive Quality Modeling for MDF Manufacturing Using Industrial Process Data and Machine Learning

Roberto Aedo-García <sup>1,\*</sup>, Miguel A. C. Valdebenito-Chavez <sup>2</sup>, Silvia E. Restrepo-Medina <sup>3,4</sup>,  
Gerson Rojas Espinoza <sup>5</sup>, Javier Zarate Bertoglio <sup>6</sup> and Francisco Ramis-Lanyon <sup>2,\*</sup>

<sup>1</sup> Departamento de Física, Facultad de Ciencias, Universidad del Bío-Bío, Av. Collao 1202, Concepción 4051381, Chile

<sup>2</sup> Departamento de Ingeniería Industrial, Facultad de Ingeniería, Universidad del Bío-Bío, Av. Collao 1202, Concepción 4051381, Chile

<sup>3</sup> Departamento de Ingeniería Eléctrica, Universidad Católica de la Santísima Concepción, Alonso de Ribera 2850, Concepción 4090541, Chile; srestrepo@ucsc.cl

<sup>4</sup> Centro de Energía, Universidad Católica de la Santísima Concepción, Alonso de Ribera 2850, Concepción 4090541, Chile

<sup>5</sup> Departameto de Ingeniería de Procesos y Bioproductos, Facultad de Ingeniería, Universidad del Bío-Bío, Av. Collao 1202, Concepción 4051381, Chile; grojas@ubiobio.cl

<sup>6</sup> Departamento de TI, Empresa Packing Bio Bio, Av. Oriental N° 6161, Peñalolén 7910000, Chile; gerenteti@pbb.cl

\* Correspondence: raedogar@ubiobio.cl (R.A.-G.); framis@ubiobio.cl (F.R.-L.)

† These authors contributed equally to this work.

## Highlights

**Please indicate how your work links to systems science via your contributions to systems practice, theory, and/or methodology.**

- The study conceptualizes continuous MDF manufacturing as a coupled multi-stage system in which disturbances propagate across drying, resin application, forming, and pressing before affecting final product quality.
- It introduces a transferable systems methodology that integrates industrial sensing, target-specific data processing, automated machine learning, and inspection planning within a unified quality-assurance framework.

**What are the main findings and/or the implications of the main findings?**

- The Vertical Density Profile index (VSC) was predicted consistently for both product families, with test RMSE values of 1.39 and 1.78 index units, whereas Internal Bond prediction depended strongly on product configuration and sensor observability.
- The models can prioritize production intervals for targeted destructive testing, supporting earlier detection of quality drift and faster corrective action without replacing formal laboratory verification.



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## Abstract

Continuous medium-density fiberboard (MDF) production presents a persistent quality-assurance problem: destructive laboratory tests return results too late to prevent off-specification material from accumulating before a corrective response is possible. This study develops an inspection-oriented predictive quality framework using industrial Distributed Control System (DCS) data and automated machine learning, treating the production line as an integrated nine-stage system in which upstream process disturbances propagate through coupled thermomechanical and chemical operations before becoming visible in final panel

properties. Two quality targets were modeled across Ultralight (UL) and Standard Thin (STD) panels using 3365 production batches and 327 DCS process variables. The pipeline combined Random Forest imputation, Pearson collinearity filtering ( $|r| \geq 0.8$ ), target-specific feature selection, and stacked ensemble regression via H2O AutoML. The Vertical Density Profile Index (VSC), a plant-reported scalar derived from X-ray density profiling, was predicted accurately in both product families (test RMSE: 1.39 and 1.78, index units for UL and STD respectively), reflecting its close coupling to drying stability, resin dosing, and thermal conditions. Internal Bond strength (IB) was harder to predict, especially for thin STD panels (test RMSE: 78.93 kPa vs. 27.41 kPa for UL), as core-layer bonding mechanisms are only indirectly observable through standard DCS instrumentation. Model-agnostic feature importance rankings were physically coherent across both product families, with dominant predictors concentrated in drying, resin application, forming, and hot pressing, consistent with the coupled-subsystem nature of MDF quality formation. The historical dataset was dominated by acceptable and over-quality IB production, which precluded conformity classification and sampling-reduction analysis; a prospective dataset with near-threshold observations is required for those evaluations. Within that scope, the framework provides continuous quality estimates, identifies deviations from the desired operating range, and supports inspection planning as a complement to formal laboratory testing.

**Keywords:** medium-density fiberboard (MDF); predictive quality control; automated machine learning (AutoML); stacked ensemble; distributed control system (DCS); inspection-oriented decision support; wood-based panels; Industry 4.0

## 1. Introduction

The medium-density fiberboard (MDF) industry has changed substantially over recent decades due to increasing requirements for product performance, resource efficiency, and raw-material diversification. Production systems that were originally designed for relatively uniform softwood fibers bonded with urea–formaldehyde resin now process a broader range of furnish types, including fast-growing hardwoods, recycled fibers, production residues, and other lignocellulosic materials. These changes support circular-economy and sustainability objectives, but they also increase variability in fiber geometry, chemical composition, bulk density, and moisture content [1–3].

Furnish variability affects fiber formation, adhesive distribution, drying behavior, and heat and mass transfer during hot pressing. Differences in fiber surface chemistry, fines content, moisture, and compressibility modify resin-curing kinetics and the development of the vertical density profile. These effects are subsequently reflected in critical product attributes such as internal bond strength (IB), bending performance, dimensional stability, and thickness swelling [4–6]. The incorporation of recycled raw materials, functional additives, and phase-change materials may further increase the number of interactions that must be controlled during production [1,6].

Continuous MDF manufacturing is therefore better represented as a coupled multi-stage system than as a collection of independent unit operations. Material passes sequentially through fiber preparation, chemical application, drying, forming, pre-pressing, hot pressing, cooling, and finishing operations. Disturbances introduced in an upstream stage may persist, interact with subsequent operating conditions, or become detectable only after the final board has been produced. Final quality consequently emerges from the complete material trajectory through the production line rather than from a single process variable or isolated machine setting [7,8].

From this perspective, MDF quality can be formulated as a latent and partially observed product state. Properties such as IB are not measured continuously during pressing and are known directly only after destructive laboratory testing. During production, the available information consists of indirect and distributed measurements of the conditions under which the material is transformed. These measurements include temperatures, pressures, moisture-related variables, flow rates, resin-dosing signals, equipment loads, and line-speed records. The quality state is only partially observed because some mechanisms that directly influence panel performance, including core temperature, local resin distribution, mat-moisture gradients, and vertical density development, may not be measured online.

Industry 4.0 technologies provide the infrastructure required to analyze this distributed process information. Distributed Control Systems (DCS), Supervisory Control and Data Acquisition systems, and programmable logic controllers continuously record high-dimensional process histories that can be associated with laboratory measurements and production records [8,9]. Within this context, Predictive Quality (PQ) refers to the estimation of product-quality characteristics from manufacturing data before or without an immediate direct measurement of the final property [10]. The resulting estimates can support process monitoring, quality-risk assessment, and decisions concerning when additional inspection is required.

Machine-learning methods are suitable for PQ applications because they can represent nonlinear relationships and interactions among a large number of process variables [9,11,12]. However, predictive performance alone is insufficient for industrial quality assurance. A model may obtain a low average regression error while failing to identify observations close to a product specification limit. Similarly, a model evaluated using randomly partitioned data may produce optimistic results when temporally adjacent production records share raw materials, operating recipes, environmental conditions, and slowly varying equipment states. For industrial deployment, predictive quality models should therefore be evaluated in relation to time, product specifications, model interpretability, and the operational cost of incorrect inspection decisions [10,13].

In MDF production, IB is a particularly important and difficult quality attribute. IB represents tensile resistance perpendicular to the board faces and is influenced by inter-fiber contact, resin distribution, core-layer curing, moisture transport, pressing conditions, and the vertical density profile. Its standard assessment requires destructive testing of specimens taken from completed panels. The resulting measurement is discrete and delayed relative to the continuous production process, limiting the speed with which quality deviations can be identified and corrected. Vertical Density Profile Index (VSCI), the second quality response considered in this study, provides complementary information related to material and thermal-process conditions. The two responses therefore represent different levels of observability from routinely recorded process data.

Previous studies have demonstrated that properties of MDF and other wood-based panels can be predicted from laboratory or industrial process variables. André et al. [14] used real plant data, multivariate calibration methods, and genetic-algorithm-based variable selection to predict MDF internal bond strength. Subsequent work developed real-time process models for particleboard properties using variable-selection and regression-ensemble methods [15]. Schubert et al. [16] combined machine and process-control variables with laboratory measurements to predict mechanical properties of industrial wood-fiber insulation boards using Random Forest, artificial neural networks, and support vector machines. Other studies have used artificial neural networks to estimate physical or mechanical properties of MDF and related wood composites [17,18].

More recently, Phetkaew et al. [19] proposed an adaptive controller framework for particleboard manufacturing that combines relevance analysis, pass/fail classification, and

decision-tree rules for process adjustment. This study is particularly relevant because it moves beyond continuous-property regression and relates process variables to conformity-oriented decisions. In manufacturing more generally, predictive model-based quality-inspection architectures have integrated data acquisition, preprocessing, model development, and industrial deployment [13]. Automated machine learning has also been investigated as a mechanism for reducing the manual effort required to compare preprocessing strategies, algorithms, and hyperparameters in predictive-quality applications [20]. Consequently, applying H2O AutoML to MDF data is not, by itself, the methodological novelty of the present study.

Table 1 summarizes the principal differences between representative studies and the proposed framework. The comparison shows that previous research has addressed several individual components, including prediction from industrial data, variable selection, non-linear modeling, pass/fail classification, and predictive-inspection architectures. However, the reviewed literature does not jointly document, for continuous MDF manufacturing, material-oriented temporal alignment across multiple coupled process areas, product-family- and target-specific modeling, chronologically ordered validation, interpretation of the selected final model, evaluation near product-acceptance limits, and simulation of inspection-oriented sampling decisions.

The main research gap is not the lack of machine-learning applications in wood-product manufacturing, but the absence of an integrated framework that connects process-to-product traceability, temporally valid prediction, physically interpretable process information, and evaluation against industrial acceptance criteria in continuous MDF production. A model intended to support inspection must therefore do more than estimate a continuous quality response. It must also identify production intervals that require additional laboratory attention while controlling the risk of missing non-conforming material. To address this gap, this study develops an inspection-oriented predictive-quality framework using industrial DCS and laboratory data. The production line is represented as nine coupled subsystems, and separate models are developed for the Ultralight and Standard Thin product families and for the IB and VSC quality responses. The analysis examines the predictive capacity of routinely recorded multistage variables under chronological validation, the stability and physical consistency of the most relevant process predictors, and the ability of the models to detect production near or outside acceptance limits. H2O AutoML is used as a controlled model-search environment within this workflow and is not considered the primary scientific contribution. The contribution of the study is threefold. Conceptually, MDF quality is represented as a latent and partially observed product state that develops along the material trajectory through coupled thermal, mechanical, and chemical operations. Methodologically, the framework integrates temporal association between process signals and laboratory samples, product- and target-specific modeling, chronological validation, interpretation of the selected final model, and threshold-based evaluation. Operationally, continuous quality predictions are converted into a rule for prioritizing destructive tests and are assessed through sensitivity, false-negative rate, potential sampling reduction, and relative inspection cost. The framework is intended to complement process supervision and formal quality assurance, rather than replace mandatory conformity testing. The central premise is that routinely acquired process variables contain sufficient information to estimate selected MDF quality properties before laboratory results become available. These estimates can support earlier identification of quality drift and more targeted process adjustment when interpreted together with engineering knowledge. The remainder of this paper is organized as follows. Section 2 describes the production system, data sources, temporal alignment, preprocessing, modeling, and validation procedures. Section 3 presents the predictive, inspection-oriented, and model-interpretation results. Section 4 discusses their physical and operational implications, and Section 5 summarizes the main findings, limitations, and future research directions.

**Table 1.** Comparison of representative predictive-quality studies relevant to wood-panel manufacturing and industrial quality inspection.

| Study                | Sector or Product            | Industrial Data | Process-Stage Coverage                                                            | Temporal Alignment                                                                     | Temporal Validation                          | Regression Metrics    | Inspection Metrics    | Sampling or Cost Evaluation                     |
|----------------------|------------------------------|-----------------|-----------------------------------------------------------------------------------|----------------------------------------------------------------------------------------|----------------------------------------------|-----------------------|-----------------------|-------------------------------------------------|
| André et al. [14]    | MDF                          | Yes             | Multiple process variables; number of physical stages not reported                | Not explicitly reported                                                                | Not explicitly reported                      | Yes                   | No                    | No                                              |
| André and Young [15] | Particleboard                | Yes             | Industrial process variables; number of physical stages not reported              | Association by manufacturing time; residence-time correction not reported              | Not explicitly reported                      | Yes                   | No                    | No                                              |
| Schubert et al. [16] | Wood-fiber insulation boards | Yes             | Machine and process variables from industrial production                          | Matched by product type and manufacturing time                                         | No explicit chronological holdout reported   | Yes                   | No                    | No                                              |
| Phetkaew et al. [19] | Particleboard                | Yes             | Process parameters analyzed within a four-step adaptive-control framework         | Association through production sampling rounds; residence-time correction not reported | Not explicitly reported                      | Limited               | Yes                   | No                                              |
| Krauß et al. [20]    | General manufacturing        | Yes             | Application-dependent predictive-quality datasets                                 | Application dependent                                                                  | Application dependent                        | Yes                   | Application dependent | No explicit sampling-cost simulation            |
| Schmitt et al. [13]  | General manufacturing        | Yes             | Integrated data acquisition, preprocessing, modeling, and deployment architecture | Application dependent                                                                  | Not explicitly reported                      | Application dependent | Yes                   | No wood-panel-specific sampling simulation      |
| Present study        | Continuous MDF               | Yes             | Nine coupled production subsystems                                                | Material-oriented alignment using process lags and aggregation windows                 | Chronological holdout and blocked validation | Yes                   | Yes                   | Sampling reduction and relative-cost simulation |

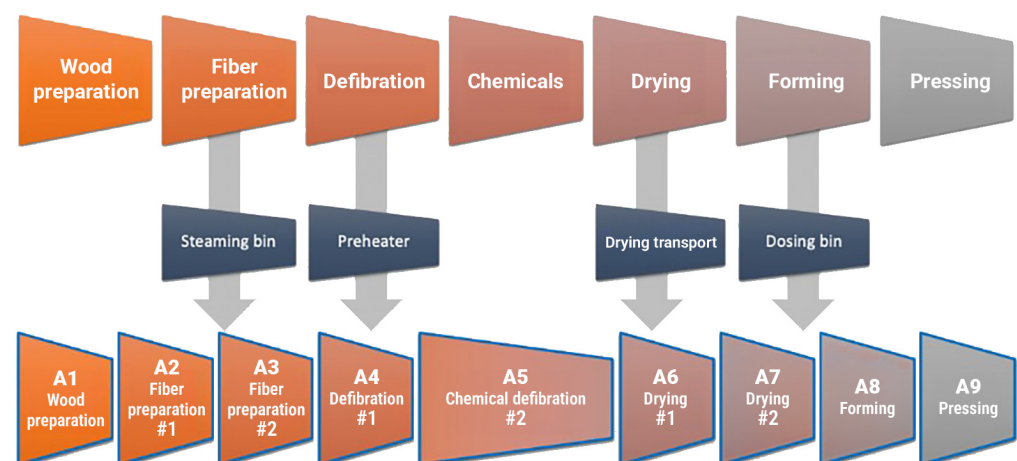
Notes: “Not explicitly reported” indicates that the corresponding methodological element could not be verified in the reviewed publication. “Application dependent” indicates that the study proposed a general framework whose implementation varied across industrial use cases. Regression metrics include measures such as RMSE, MAE, MAPE, or  $R^2$ . Inspection metrics include sensitivity, specificity, precision, and false-negative rate.

## 2. Materials and Methods

This study develops and evaluates predictive models for key quality attributes in continuous MDF manufacturing using industrial process data. The methodological framework integrates plant-level data acquisition, preprocessing, target-specific feature selection, temporal consistency criteria, and supervised machine learning. The MDF production line is treated as a continuous, multi-stage manufacturing system in which upstream disturbances propagate through interconnected thermomechanical and chemical operations before becoming visible in final panel properties. Traceability between process signals, material transformation, and inspection-oriented quality outcomes is maintained at each methodological step.

### 2.1. Industrial MDF Manufacturing Process Description

Industrial MDF production is a continuous sequence of thermomechanical, chemical, and forming operations that transform raw logs into consolidated panels. The production line analyzed here comprises nine operational stages (A1–A9), shown in Figure 1, which map directly to the plant’s Distributed Control System (DCS) architecture. This structure provides traceability between process zones and historical sensor records.



**Figure 1.** Schematic flow diagram of the medium-density fiberboard (MDF) manufacturing process (A1–A9) analyzed in this study.

The complete process historian contains 327 TAGs distributed across the nine stages, used for online monitoring, process stabilization, and defect prevention. For this study, the MDF line was defined as the manufacturing system bounded by raw material preparation at the inlet and panel release after pressing at the outlet. Main system inputs are raw wood material, steam, thermal energy, and resin-additive formulations; primary outputs are finished MDF panels and their associated quality measurements. Process TAGs serve as observable-state descriptors of the system, while laboratory quality variables provide delayed-response measurements for supervised model development. A complete dictionary of the process tags, including the original plant identifier, a descriptive label, and the coded variable name used during modeling, is provided in Appendix A.

The nine operational stages are summarized below:

- **A1. Wood Preparation:** Raw logs are received, sorted, and conditioned to provide stable feedstock for downstream processing. This stage is monitored by 17 variables and is relevant to limiting variability that may later affect fiber geometry, furnish consistency, and density formation.
- **A2–A3. Fiber Preparation #1 and #2:** Chips undergo size reduction in A2 (21 variables) and thermal conditioning in A3 (10 variables), typically under saturated steam, to improve refining efficiency and fiber softening.

- **A4. Defibration:** Steam-conditioned chips are mechanically refined into fibers. This stage is monitored by 16 variables associated with refining intensity and stock consistency, both of which are relevant for downstream mat formation and bonding behavior.
- **A5. Chemical Defibration #2:** Fibers are blended with urea–formaldehyde (UF) resin and additives. This stage, monitored by 70 variables, regulates dosing, mixing conditions, and temperature, thereby playing a central role in bond formation and panel integrity.
- **A6–A7. Drying #1 and #2:** Moisture is reduced in two consecutive stages to values suitable for the formation and hot pressing. A total of 57 variables describe airflow, temperature, and related operating conditions that affect drying stability and final moisture distribution.
- **A8. Forming:** Resin-treated fibers are distributed to form a mat with controlled basis weight. This stage is monitored by 22 variables related to feeding stability and cross-machine uniformity, which influence the subsequent density profile.
- **A9. Pressing:** The mat is consolidated in a continuous hot press, where densification and resin curing take place. This stage is described by 114 variables, including platen position, thermal conditions, and compression dynamics, and is directly linked to thickness control, curing effectiveness, and delamination risk.

After pressing, panels are discharged for grading and storage. Because final product properties emerge from interactions across all stages, the MDF line is analyzed as an interconnected production system rather than a set of independent unit operations.

## 2.2. Panel Classes and Process Context

The study covers two commercial MDF product families manufactured on the same continuous line: Ultralight (UL) and Standard Thin (STD). UL panels are produced at densities below  $600 \text{ kg}\cdot\text{m}^{-3}$ , reducing mass while meeting mechanical requirements for non-structural interior applications such as cabinet backings and door skins [3,6]. STD panels correspond to conventional MDF densities, typically within  $650$  to  $750 \text{ kg}\cdot\text{m}^{-3}$ , but are produced at reduced thicknesses in the range of 2 to 6 mm, prioritizing dimensional precision, surface quality, and machinability for lamination-oriented products (cf. [21]).

Both families pass through the same unit operations: defibration, drying, resin blending, mat forming, and continuous hot pressing. Their density-thickness combinations and target operating windows differ, however, which affects how process variability translates into final board properties. This contrast makes the two families useful for evaluating whether similar process signals retain predictive value across distinct manufacturing regimes.

## 2.3. Laboratory Quality Measurements

Two laboratory-measured quality responses were analyzed: Internal Bond strength (IB) and the Vertical Density Profile Index (VSC). Both responses were obtained from routine production-quality records associated with the corresponding MDF production intervals. The laboratory results, rather than model predictions, remained the reference measurements for product conformity assessment.

### 2.3.1. Internal Bond Strength Measurement

Internal Bond strength quantifies the tensile resistance of the panel perpendicular to its faces and serves as an indicator of core-layer bonding and resin-curing effectiveness. The test was conducted according to EN 319 or ASTM D1037 [22,23] using specimens cut from the corresponding panel sampling location. Loading blocks were bonded to both faces, and the specimens were loaded perpendicular to the panel surfaces until failure. Internal Bond strength was calculated as:

$$IB = \frac{F_{\max}}{A}, \quad (1)$$

where  $F_{\max}$  is the maximum tensile force recorded at failure (N) and  $A$  is the loaded cross-sectional area (mm<sup>2</sup>). Results were converted to kPa for modeling and reporting.

The applicable lower acceptance limits were 470 kPa for Ultralight panels and 700 kPa for Standard Thin panels. Values below the corresponding limit were classified as non-conforming.

### 2.3.2. Vertical Density Profile Index Measurement

In this study, VSC is the identifier used in the plant quality system for the index associated with the vertical density profile of the MDF panel. It does not represent Volatile Solids Content, moisture loss, resin volatility, or any other gravimetric or chemical measurement. The underlying measured property is the variation in local panel density through the complete panel thickness.

The vertical density profile was determined off-line using a laboratory X-ray density profiler manufactured by GreCon (Fagus-GreCon Greten GmbH & Co. KG, Alfeld, Germany). A representative specimen containing the complete panel thickness was extracted from the MDF panel submitted for routine quality control. The specimen was positioned so that the X-ray system scanned sequentially from one panel face to the opposite face. Consequently, the measurement direction was perpendicular to the panel plane and coincident with the thickness direction.

Let  $h_i$  denote the measured thickness of specimen  $i$ , and let  $z \in [0, h_i]$  denote the position through its thickness. During the scan, the instrument recorded the transmitted X-ray intensity at a sequence of positions  $z_j$ . The attenuation signal was expressed conceptually as

$$A_i(z_j) = \ln \left( \frac{I_{0,r}}{I_i(z_j)} \right), \quad (2)$$

where  $I_{0,r}$  is the reference X-ray intensity for the active instrument calibration or product recipe  $r$ , and  $I_i(z_j)$  is the intensity transmitted through the specimen at position  $z_j$ . The GreCon calibration routine converted attenuation into local density according to

$$\rho_i(z_j) = C_r [A_i(z_j)], \quad (3)$$

where  $\rho_i(z_j)$  is the local density, expressed in kg m<sup>-3</sup>, and  $C_r$  denotes the equipment calibration function applicable to the panel type, nominal thickness, and measurement configuration.

The complete vertical density profile for specimen  $i$  was therefore represented as

$$\text{VDP}_i = \{ (z_j, \rho_i(z_j)) \}_{j=1}^{N_i}, \quad (4)$$

where  $N_i$  is the number of measurement positions generated during the scan. The GreCon software displayed and stored this result as a curve of local density versus position through the panel thickness. This curve captures the high-density surface regions, the transition zones, and the lower-density core region that develop during hot pressing.

For the predictive analyses, the response denoted as VSC was the scalar profile index recorded in the plant quality database and linked to the corresponding GreCon density-profile measurement. The index can be represented as

$$\text{VSC}_i = \mathcal{G}_r(\text{VDP}_i), \quad (5)$$

where  $\mathcal{G}_r$  is the profile-processing routine configured in the plant quality-control system for product recipe  $r$ . The value exported by this routine was used directly as the response vari-

able. No additional normalization, mass-loss calculation, thermal treatment, or chemical transformation was applied during preparation of the modeling dataset.

The raw density profile and the reported VSC index represent different levels of the same measurement. The raw profile has physical units of  $\text{kg m}^{-3}$  and retains the spatial distribution of density through the panel thickness. VSC is a unitless plant index that summarizes the measured profile for routine monitoring and historical comparison. It must therefore be interpreted relative to the applicable panel family and product recipe rather than as an absolute density or a material concentration.

The profile is industrially relevant because its shape reflects mat consolidation, heat and moisture transfer, press closing behavior, and density development during hot pressing. High-density surface layers generally contribute to bending stiffness and strength, whereas the density and integrity of the core region are particularly relevant to internal bond strength. Accordingly, VSC was used as an indicator of through-thickness density development and not as a substitute for a specific mechanical test.

VSC was modeled as a continuous response. No universal external pass/fail limit exists for this plant-specific index. For the error-stratified analyses, observations were separated into low, central, and high VSC bands using the first and third quartiles calculated independently for each product family:

$$B_i = \begin{cases} \text{low VSC,} & \text{VSC}_i < Q_{0.25,p}, \\ \text{central VSC,} & Q_{0.25,p} \leq \text{VSC}_i \leq Q_{0.75,p}, \\ \text{high VSC,} & \text{VSC}_i > Q_{0.75,p}, \end{cases} \quad (6)$$

where  $p$  identifies the panel family and  $Q_{0.25,p}$  and  $Q_{0.75,p}$  are the corresponding empirical quartiles. These bands were used solely to examine whether prediction errors changed across the observed VSC range. They were not treated as regulatory conformity limits or as replacements for the plant's controlled product specifications.

Table 2 summarizes the measurement basis, reported scale, and industrial interpretation of the two quality responses used in the predictive analysis.

**Table 2.** Definition and industrial interpretation of the quality responses used in the predictive models.

| Response | Measured Property                                                                        | Laboratory Procedure                                                                                                                                                                                                                                                                                                  | Reported Scale                                                                  | Analysis Rule                                                                                                                                 | Practical Interpretation                                                                                                                                                                                          |
|----------|------------------------------------------------------------------------------------------|-----------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|---------------------------------------------------------------------------------|-----------------------------------------------------------------------------------------------------------------------------------------------|-------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|
| IB       | Tensile strength perpendicular to the panel faces                                        | A specimen extracted from the finished MDF panel was bonded to loading blocks and subjected to tensile loading perpendicular to the panel plane until failure.                                                                                                                                                        | kPa                                                                             | Continuous response; product conformity is assessed against the applicable product-specific lower limit.                                      | Low values indicate insufficient bonding or curing in the panel core and may be associated with unfavorable core-density development.                                                                             |
| VSC      | Plant-reported index derived from the vertical density profile of the finished MDF panel | A full-thickness specimen was scanned perpendicular to the panel plane using a GreCon X-ray density profiler. Calibrated X-ray attenuation was converted into local density, producing a density-versus-thickness curve. The scalar VSC value stored in the quality database was used without further transformation. | Unitless plant index; underlying profile in $\text{kg m}^{-3}$ versus thickness | Continuous response. Product-specific empirical quartiles were used only to stratify prediction errors into low, central, and high VSC bands. | Describes through-thickness density development, including the surface density peaks, transition regions, and core-density zone formed during hot pressing. It is not a volatile-solids or mass-loss measurement. |

For both Ultralight and Standard Thin panels, the VSC index ranged from approximately 80 to 100 across the training subset.

#### 2.4. Data Acquisition and Experimental Context

Historical operational records from an industrial MDF facility were consolidated into a dataset of 3365 production batches and 356 variables, classified into three groups:

- **Temporal variables** (10): timestamp-related variables used for process traceability and exploratory inspection but excluded from predictive training.
- **Quality variables** (19): laboratory-derived product measurements considered as candidate response variables.
- **Process variables** (327): DCS TAGs recorded across the nine production zones (A1–A9), identified using the notation  $A_{i,j}$ , where  $i$  denotes the process area and  $j$  the sensor identifier.

Data auditing revealed extensive missingness in several laboratory quality variables, attributable to selective testing practices, particularly in UL production cycles. Variables including MOE, MOR, Water Absorption, and Thickness Swelling showed missingness rates above 68%. Under a conventional 70/20/10 split, these variables would yield test subsets too small for reliable generalization assessment and were therefore excluded from the modeling scope. Missing values in process predictors were handled by Random Forest (RF)-based multivariate imputation, selected for its ability to preserve nonlinear dependencies among industrial variables without imposing distributional assumptions that are rarely appropriate in MDF process data. Imputation was applied only to predictor variables; quality responses were never imputed, preventing leakage of laboratory information into the feature space.

For UL panels, 47 process variables required imputation. A Pearson collinearity filter with threshold  $|r| \geq 0.8$  then removed 129 redundant predictors, leaving a candidate set of 154 variables (Table 3). For STD panels, 42 variables required imputation and 137 collinear predictors were removed, leaving 148 variables (Table 4).

The threshold  $|r| \geq 0.8$  was chosen as a conservative criterion that reduces redundancy while retaining complementary information. In industrial environments, highly correlated TAGs typically reflect shared actuators, derived variables, or common control loops. Removing them improves numerical stability and interpretability without eliminating the capacity of ensemble or neural methods to capture nonlinear process interactions.

**Table 3.** Missing data and collinearity reduction summary for Ultralight (UL) panels.

| Preprocessing Step       | Affected Variables | Method/Threshold         | Outcome                      |
|--------------------------|--------------------|--------------------------|------------------------------|
| Missing Data             | 47 variables       | Random Forest Imputation | All missing values estimated |
| Collinearity Filter      | 129 variables      | Pearson $ r  \geq 0.8$   | Removed from feature space   |
| Post-filter Variable Set | 154 variables      | –                        | Retained for modeling        |

Variables correspond mainly to process signals from hot pressing, resin application, and drying sections.

**Table 4.** Missing data and collinearity reduction summary for Standard Thin (STD) panels.

| Preprocessing Step       | Affected Variables | Method/Threshold         | Outcome                      |
|--------------------------|--------------------|--------------------------|------------------------------|
| Missing Data             | 42 variables       | Random Forest Imputation | All missing values estimated |
| Collinearity Filter      | 137 variables      | Pearson $ r  \geq 0.8$   | Removed from feature space   |
| Post-filter Variable Set | 148 variables      | –                        | Retained for modeling        |

Variables correspond mainly to process signals from hot pressing, resin application, and drying sections.

### 2.5. Exploratory Data Analysis and Variable Selection

Exploratory analysis and feature screening were conducted separately for UL and STD panels to preserve the distinction between product classes and their operating regimes. Although the plant historian stores 327 DCS TAGs, class-specific candidate sets were smaller because some signals were inactive, quasi-constant, or inconsistently recorded during particular campaigns. After this screening, UL models started from 283 candidate predictors and STD models from 285. A comparative summary of the preprocessing and target-specific feature selection results is presented in Table 5.

**Table 5.** Comparative preprocessing and target-specific feature selection for UL and STD MDF panels.

| Feature                      | Ultralight (UL) | Standard Thin (STD) |
|------------------------------|-----------------|---------------------|
| Initial candidate predictors | 283             | 285                 |
| Post-collinearity predictors | 154             | 148                 |
| Collinear variables removed  | 129             | 137                 |
| Predictors imputed (RF)      | 47              | 42                  |
| Final IB predictors          | 55              | 56                  |
| Final VSC predictors         | 72              | 75                  |
| Top correlated tag (IB)      | 0.31 (A9_24)    | A9_53               |
| Top correlated tag (VSC)     | 0.32 (A6_29)    | —                   |

The preprocessing pipeline was identical for both product families: RF-based imputation, Pearson collinearity filtering, and target-specific feature selection. This shared structure ensures comparability while allowing the final predictor sets to remain specific to each quality target.

For UL panels, 47 predictors required imputation and 129 collinear variables were removed, leaving 154 non-redundant predictors. Target-specific selection produced distinct feature sets for each response. For Internal Bond (IB), 56 predictors passed the correlation screen and 55 were retained after importance-based pruning; the strongest linear association was observed for A9\_24 ( $r \approx 0.31$ ). For Vertical Density Profile Index (VSC), 72 predictors met the screening criterion and were retained, with A6\_29 showing the strongest linear association ( $r \approx 0.32$ ).

For STD panels, 42 predictors were imputed and 137 collinear variables removed, yielding 148 predictors. For IB, 60 predictors passed the correlation screen and 56 remained after importance-based filtering, with A9\_53 among the most relevant contributors. For VSC, 77 predictors were initially selected and 75 retained after pruning. The quality targets depend on partially overlapping but non-identical subsets of process signals. VSC is associated with a broader set of process conditions than IB within the screened variable space. The strongest pairwise correlations remained modest ( $|r| \approx 0.31$  to  $0.32$ ), consistent with quality outcomes that arise from coupled process interactions rather than any single dominant sensor signal. Correlation screening served exclusively as an initial dimensionality-reduction step, not as evidence of direct causality. Variable retention was interpreted in operational and predictive terms: identifying potentially informative signals prior to multivariate model fitting.

### 2.6. Temporal Alignment and Material Tracking in Continuous Production

In continuous MDF manufacturing, process variables must be associated with the same material segment that is subsequently evaluated in the laboratory. Measurements generated during wood preparation, refining, chemical application, drying, forming, and pressing occur at different times, although they describe successive transformations of the same product. An incorrect temporal association may therefore link a laboratory result

to process conditions belonging to another production interval and reduce the physical validity of the predictive model.

Previous studies have shown that upstream variables such as refining conditions, motor load, and energy consumption can provide early information about downstream product properties [7,24,25]. Variables related to mat consolidation, press geometry, panel thickness, and density development have also been associated with mechanical quality [7,26,27]. Similarly, surface roughness, drilling response, water absorption, and thickness swelling retain information from previous machining, additive-dosing, and pressing conditions [28–30]. These findings support a material-oriented alignment procedure rather than direct matching based only on the laboratory timestamp.

For each laboratory observation, the material trajectory was reconstructed backward from the timestamp recorded by the Human–Machine Interface (HMI) at the continuous press. This reference time was denoted by  $t_1$ . The estimated passage times through the upstream process areas,  $t_2, \dots, t_9$ , were calculated recursively using known transport distances, nominal residence times, press-belt speed, and dosing-bin level.

The timestamp associated with the forming section was calculated from the distance to the press:

$$t_2 = t_1 - \frac{L_{\text{forming}}}{v_{\text{press},i}} \times 60, \quad (7)$$

where  $L_{\text{forming}} = 100$  m and  $v_{\text{press},i}$  is the press-belt speed for production record  $i$ , expressed in  $\text{m min}^{-1}$ . The factor 60 converts the calculated travel time to seconds.

The delay associated with the second drying section was adjusted using the recorded dosing-bin level:

$$t_3 = t_2 - 600 \left( \frac{B_i}{100} \right), \quad (8)$$

where  $B_i$  is the dosing-bin level expressed as a percentage. The division by 100 converts the recorded value to a fraction between 0 and 1.

The remaining upstream timestamps were calculated using fixed transport or residence-time corrections:

$$t_4 = t_3 - 120, \quad (9)$$

$$t_5 = t_4 - 15, \quad (10)$$

$$t_6 = t_5 - (3.3 \times 60), \quad (11)$$

$$t_7 = t_6 - 20, \quad (12)$$

$$t_8 = t_7 - 420, \quad (13)$$

$$t_9 = t_8 - 30. \quad (14)$$

The fixed delays in Equations (9)–(14) were derived from nominal transport distances and residence times documented in the plant engineering records, not from data-driven lag optimization. All delays in Equations (9)–(14) are expressed in seconds. The reconstructed timestamps correspond, respectively, to Drying #1, Refining #2 and chemical addition, Refining #1, Fiber Preparation #2, Fiber Preparation #1, and Wood Preparation.

For process area  $a$ , the reconstructed timestamp  $t_{i,a}$  was used as the temporal reference for laboratory sample  $i$ . The associated aggregation interval was defined as

$$W_{i,a} = [t_{i,a} - \Delta_a^-, t_{i,a} + \Delta_a^+], \quad (15)$$

where  $\Delta_a^-$  and  $\Delta_a^+$  denote the backward and forward limits of the area-specific window. DCS observations contained within this interval were assigned to the corresponding material segment. For continuously sampled variable  $j$ , the representative value was calculated as

$$\bar{x}_{i,j} = \frac{1}{n_{i,a}} \sum_{t \in W_{i,a}} x_j(t), \quad (16)$$

where  $x_j(t)$  is the recorded DCS signal and  $n_{i,a}$  is the number of valid measurements within the aligned interval. Variables already stored as batch-level statistics in the production database were used without additional temporal averaging.

The alignment procedure was based on engineering residence-time relations rather than data-driven lag optimization. Correlation-based methods, including cross-correlation, distance correlation, and maximal information coefficient, can be useful when physical residence times are unknown [31]. In this study, however, they were not used to replace the known production-sequence relationships. This choice preserves the physical interpretation of the aligned predictors and avoids selecting temporal delays solely according to their association with the target variable.

Production intervals identified as stoppages, start-ups, incomplete production cycles, or product transitions were excluded when a consistent material trajectory could not be established. No temporal interpolation was performed across these intervals. Records with incomplete timestamp sequences or insufficient DCS coverage within the corresponding aggregation window were also removed. Ultralight and Standard Thin observations were subsequently modeled separately to avoid combining distinct operating regimes.

This treatment is relevant because stoppages and transitions may produce valid sensor readings that do not represent stable material flow [24]. The resulting predictor vectors therefore represent physically consistent sequences of operating conditions experienced by the material before laboratory testing.

For long-term deployment, temporal alignment must be complemented by dataset versioning, operating-mode labeling, and monitoring of missing data and process drift. Structured real-time data pipelines facilitate model traceability and iterative updating in cyber-physical and digital-twin environments [32]. Changes in raw materials, recipes, equipment condition, or sensor calibration may produce temporal performance degradation and should be monitored during industrial operation [33,34].

## 2.7. Data Partition and Distributional Assessment

For each product family and quality response, the available observations were randomly divided into training, validation, and test subsets using proportions of 70%, 20%, and 10%, respectively. The partition was performed independently for each product–target combination. The resulting sample sizes were 1189/329/162 for Ultralight IB, 1195/327/158 for Ultralight VSC, 489/157/69 for Standard Thin IB, and 502/146/67 for Standard Thin VSC in the training, validation, and test subsets, respectively.

To determine whether random allocation produced systematic differences in the marginal distributions of the quality responses, the training, validation, and test subsets were compared using complementary non-parametric procedures. Pairwise two-sample Kolmogorov–Smirnov tests were used to compare the complete empirical distributions, the Kruskal–Wallis test was used to assess differences in central location, and the Brown–Forsythe test was used to evaluate differences in dispersion.

For subsets  $g$  and  $h$ , the Kolmogorov–Smirnov statistic was defined as

$$D_{g,h} = \sup_y |F_g(y) - F_h(y)|, \quad (17)$$

where  $F_g(y)$  and  $F_h(y)$  are the corresponding empirical cumulative distribution functions.

Differences in central location were evaluated using the Kruskal–Wallis statistic,

$$H = \frac{12}{N(N+1)} \sum_{g=1}^G \frac{R_g^2}{n_g} - 3(N+1), \quad (18)$$

where  $G = 3$  represents the training, validation, and test subsets,  $n_g$  is the number of observations in subset  $g$ ,  $R_g$  is the sum of ranks in that subset, and  $N = \sum_{g=1}^G n_g$ .

Dispersion was assessed using the Brown–Forsythe transformation,

$$z_{ig} = |y_{ig} - \tilde{y}_g|, \quad (19)$$

where  $y_{ig}$  is observation  $i$  in subset  $g$ , and  $\tilde{y}_g$  is the corresponding group median. An analysis of variance was then applied to the transformed values  $z_{ig}$ .

For all tests, the null hypothesis stated that the corresponding distributional characteristic did not differ among subsets. A significance level of  $\alpha = 0.05$  was adopted. The inferential analysis was complemented by comparisons of the mean, median, standard deviation, interquartile range, and observed range of IB and VSC.

These tests were used to assess distributional balance after random partitioning. They were not interpreted as evidence of temporal independence between adjacent production batches.

## 2.8. Model Development and Evaluation

Supervised regression models were developed to predict two laboratory-measured quality attributes in industrial MDF manufacturing: Internal Bond strength (IB, kPa) and the Vertical Density Profile Index (VSC, unitless index). In this study, VSC was treated as a plant-reported quality indicator used for industrial process monitoring rather than as a direct compositional measurement.

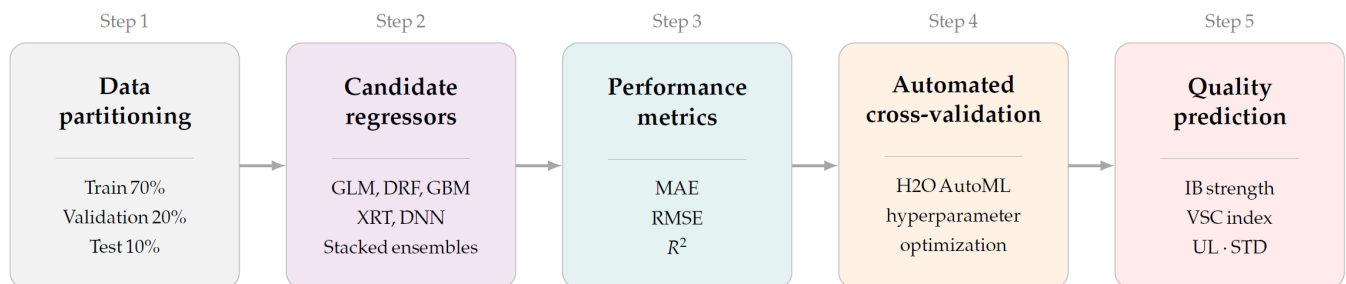
Separate models were developed for Ultralight and Standard Thin panels using production data collected between June 2017 and June 2018. The predictor set combined process measurements from nine production areas (A1–A9) with the corresponding laboratory quality observations. Because laboratory assays were recorded less frequently than the DCS signals, the modeling task involved estimating sparse quality responses from a high-dimensional process dataset.

For each product family and target variable, the curated observations were divided into training, validation, and test subsets using proportions of 70%, 20%, and 10%, respectively, as described in Section 2.7. The training subset was used to fit candidate models, the validation subset was used for model comparison and selection, and the test subset was reserved for the final hold-out evaluation.

Model development was conducted using the H2O AutoML (version 3.42, H2O.ai, Mountain View, CA, USA) framework [35]. The candidate model family included Gradient Boosting Machines (GBM), Distributed Random Forests (DRF), Extremely Randomized Trees (XRT), Deep Neural Networks (DNN), and Generalized Linear Models (GLM). AutoML also generated stacked ensembles by combining selected base learners through a metalearning procedure.

Candidate models were ranked using validation Root Mean Squared Error (RMSE) as the primary selection criterion. Mean Absolute Error (MAE) was used as a complementary metric to assess average prediction deviation. The selected model was determined independently for each product–target combination. A stacked ensemble was retained only when it achieved the lowest validation RMSE; otherwise, the highest-ranked individual learner was selected. Model identity and hyperparameters were fixed before predictions were generated for the test subset.

The test subset was not used for model ranking, hyperparameter adjustment, feature selection, or replacement of the selected model. Its sole purpose was to estimate the hold-out predictive performance of the model selected during the training and validation stages. The complete modeling procedure is summarized in Figure 2.



**Figure 2.** Predictive modeling workflow for MDF quality estimation using H2O AutoML. Separate models were developed for IB and VSC in Ultralight and Standard Thin panels. Candidate models were fitted using the training subset, compared using validation RMSE, and evaluated on the held-out test subset after model selection.

Predictive performance on the test subset was quantified using Mean Absolute Error (MAE), Root Mean Squared Error (RMSE), and the coefficient of determination ( $R^2$ ). MAE and RMSE were calculated as

$$\text{MAE} = \frac{1}{n} \sum_{i=1}^n |y_i - \hat{y}_i|, \quad (20)$$

$$\text{RMSE} = \sqrt{\frac{1}{n} \sum_{i=1}^n (y_i - \hat{y}_i)^2}, \quad (21)$$

and  $R^2$  was calculated as

$$R^2 = 1 - \frac{\sum_{i=1}^n (y_i - \hat{y}_i)^2}{\sum_{i=1}^n (y_i - \bar{y})^2}, \quad (22)$$

where  $y_i$  and  $\hat{y}_i$  are the observed and predicted values, respectively,  $\bar{y}$  is the mean of the observed target values in the test subset, and  $n$  is the number of test observations.

RMSE was used as the main performance metric because it gives greater weight to large prediction errors, which are relevant in industrial quality-control applications. MAE provided a complementary measure of the typical prediction error, while  $R^2$  described the proportion of response variability represented by the model.

Because the intended application is inspection support, the regression metrics were interpreted as measures of predictive error rather than as direct evidence of conformity-classification performance. The ability of the models to prioritize laboratory testing or identify non-conforming production requires a separate threshold-based evaluation using metrics such as sensitivity, specificity, precision, and false-negative rate.

To interpret the final stacked ensemble, model-agnostic permutation feature importance was calculated directly from the ensemble prediction function. For each response, the independent test set was first evaluated without perturbation. Each predictor was subsequently permuted 30 times while all remaining predictors were held unchanged. Feature importance was quantified as the mean increase in RMSE, and the standard deviation across permutations was retained as an uncertainty measure. Global SHAP values were additionally estimated using a permutation-based model-agnostic explainer with 40 training observations as the background distribution and 50 test observations for global interpretation. SHAP importance was expressed as the mean absolute contribution of each predictor. Ranking stability was evaluated by recalculating permutation importance on the training, validation and

test partitions. Pairwise Spearman correlations, Kendall's coefficient of concordance, mean rank, rank standard deviation and top-10 selection frequency were used to quantify stability.

### 3. Results

The results are presented in six parts. First, the distributional balance of the training, validation, and test subsets is examined. Second, the observed IB distributions are compared with the operating quality ranges for both product families. Third, predictive performance is reported for each product–target combination. Fourth, the error structure is evaluated across the observed quality range. Fifth, the process variables associated with model predictions are examined. Finally, the implications and limitations of the models for inspection support are discussed.

Because the data subsets were obtained through random allocation, the reported test metrics represent hold-out performance under distributionally comparable operating conditions. They should not be interpreted as prospective validation on a later production period.

#### 3.1. Distributional Balance Across Data Subsets

Table 6 presents the statistical comparison of IB and VSC across the training, validation, and test subsets.

**Table 6.** Distributional comparison of IB and VSC across the training, validation, and test subsets.

| Product | Target | Kruskal–Wallis $p$ | Brown–Forsythe $p$ | KS Train–Validation $p$ | KS Train–Test $p$ | KS Validation–Test $p$ | Interpretation                                                                           |
|---------|--------|--------------------|--------------------|-------------------------|-------------------|------------------------|------------------------------------------------------------------------------------------|
| UL      | IB     | 0.3833             | 0.9614             | 0.7444                  | 0.4595            | 0.9074                 | No significant differences in location, dispersion, or empirical distribution.           |
| UL      | VSC    | 0.6428             | <b>0.0345</b>      | 0.3764                  | 0.5765            | 0.9901                 | Comparable location and empirical distributions, with a modest difference in dispersion. |
| STD     | IB     | 0.2923             | 0.0577             | 0.4135                  | 0.1698            | 0.1901                 | No significant differences in location, dispersion, or empirical distribution.           |
| STD     | VSC    | 0.6071             | 0.7388             | 0.9720                  | 0.8088            | 0.5984                 | No significant differences in location, dispersion, or empirical distribution.           |

Notes: UL denotes Ultralight MDF, STD denotes Standard Thin MDF, and KS denotes the two-sample Kolmogorov–Smirnov test. The Kruskal–Wallis test evaluates differences in central location, whereas the Brown–Forsythe test evaluates differences in dispersion around the subset medians. Bold type identifies  $p < 0.05$ .

For Ultralight IB, none of the tests indicated significant differences among the three subsets. The Kruskal–Wallis test yielded  $p = 0.3833$ , the Brown–Forsythe test yielded  $p = 0.9614$ , and all pairwise Kolmogorov–Smirnov comparisons were non-significant. Standard Thin IB showed a similar pattern, with no significant differences in central location, dispersion, or empirical distribution.

For Ultralight VSC, the Kruskal–Wallis and pairwise Kolmogorov–Smirnov tests indicated comparable central values and empirical distributions. The Brown–Forsythe test detected a difference in dispersion ( $p = 0.0345$ ). The magnitude of this difference was limited, with standard deviations of 1.89, 1.98, and 2.08 index units for the training, validation, and test subsets, respectively.

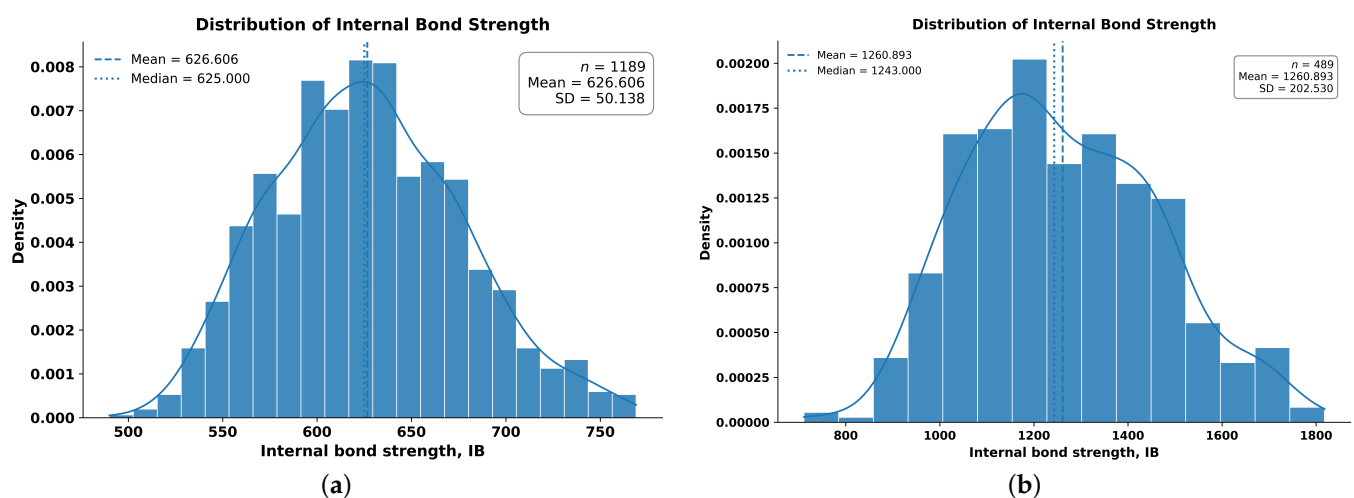
For Standard Thin VSC, none of the tests identified significant differences among the subsets. Overall, the random partition preserved similar marginal distributions of IB and VSC, with the exception of the small increase in dispersion observed for Ultralight VSC.

These findings support the use of the three subsets for model fitting, selection, and hold-out evaluation under broadly comparable response distributions. They do not demonstrate temporal independence and should not be interpreted as chronological or prospective validation.

### 3.2. IB Distribution Relative to the Operating Quality Range

The IB distributions were examined relative to the operating quality ranges used for the two MDF product families. For Ultralight panels, the reference interval was 520–600 kPa. The training subset had a mean of 626.61 kPa and a median of 625.00 kPa, placing the center of the distribution above the upper reference limit.

As shown in Figure 3, the historical IB data were concentrated mainly above the operating quality ranges. For Ultralight panels, the mean and median exceeded the upper reference limit of 600 kPa. The displacement was more pronounced for Standard Thin panels, whose mean and median were substantially higher than the upper reference limit of 870 kPa.



**Figure 3.** Distribution of Internal Bond strength relative to the operating quality ranges. (a) Ultralight MDF training subset ( $n = 1189$ ): the observed mean and median were 626.61 and 625.00 kPa, respectively, compared with an operating reference range of 520–600 kPa. (b) Standard Thin MDF training subset ( $n = 489$ ): the observed mean and median were 1260.89 and 1243.00 kPa, respectively, compared with an operating reference range of 750–870 kPa.

The observed pattern indicates that the dataset was dominated by acceptable and over-quality production rather than by recurrent low-IB events. In operational terms, the principal condition represented in the data was therefore systematic quality giveaway.

This result is relevant for process control because IB values above the required range may reflect operating conditions that are more intensive than necessary. Possible contributors include resin application, thermal input, pressing intensity, or interactions among these variables. The observational data do not support direct attribution to a specific process factor, but the distributional shift identifies a potential opportunity for process adjustment while maintaining the applicable quality requirement.

The limited number of observations near or below the lower acceptance limits also restricts a conventional conformity-classification analysis. Sensitivity, specificity, precision, and false-negative rate cannot be estimated robustly when the non-conforming class is poorly represented. For the same reason, a sampling-reduction or inspection-cost simulation would not provide a reliable estimate of the risk of missing non-conforming production.

The models are therefore interpreted in this study as continuous quality estimators and over-quality monitoring tools rather than as validated conformity classifiers. A prospective dataset containing sufficient near-threshold and non-conforming observations would be

required to assess conformity detection, destructive-sampling reduction, and inspection-cost trade-offs.

### 3.3. Predictive Performance on Held-Out Production Data

Model performance was evaluated using the randomly held-out test subset, which was excluded from model fitting, hyperparameter adjustment, and model selection. Predictive performance was quantified using Root Mean Squared Error (RMSE) and Mean Absolute Error (MAE), expressed in the native scale of each response: Internal Bond strength (IB, kPa) and Vertical Density Profile Index (VSC, unitless index).

Model benchmarking was conducted using H2O AutoML. Candidate models were fitted using the training subset and ranked independently for each product–target combination according to validation RMSE. MAE was used as a complementary metric. Once the highest-ranked candidate had been identified, its model specification was fixed and the test subset was used only for the final hold-out evaluation [10,35].

#### 3.3.1. Internal Bond Strength Prediction Performance

Table 7 identifies the model selected from the validation results for each product–target combination and reports its subsequent hold-out test performance. For Ultralight panels, the IB model achieved an RMSE of 27.41 kPa and an MAE of 18.71 kPa. For Standard Thin panels, the corresponding values were 78.93 kPa and 49.68 kPa.

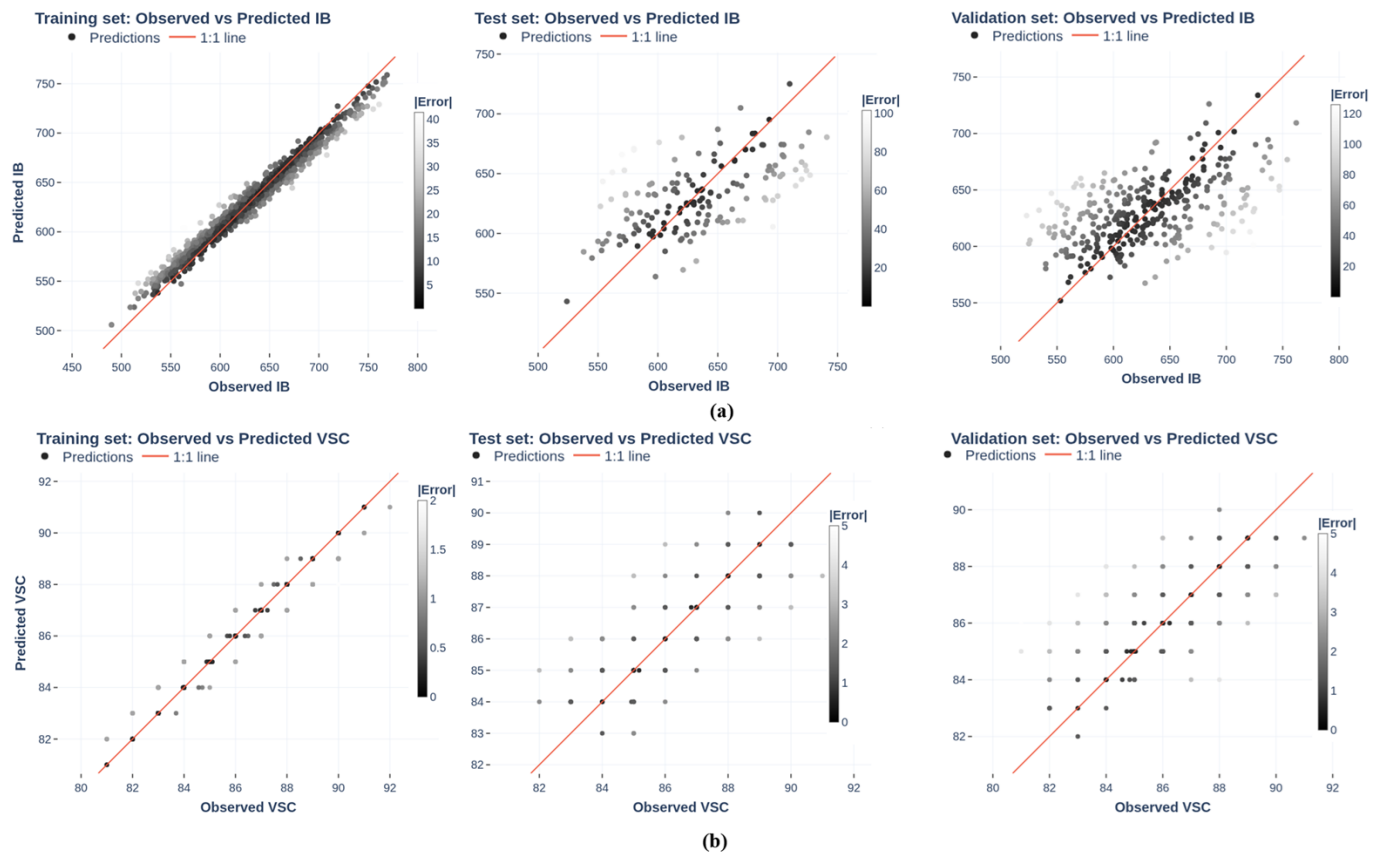
**Table 7.** Selected models and their performance on the validation and held-out test subsets. Models were ranked by validation RMSE independently for each product–target combination; the test subset was evaluated only after model selection was complete.

| Panel Type    | Target | Selected Model                                                                                                    | Val. RMSE | Val. MAE | Test RMSE | Test MAE | Test <i>n</i> |
|---------------|--------|-------------------------------------------------------------------------------------------------------------------|-----------|----------|-----------|----------|---------------|
| Ultralight    | IB     | Stacked Ensemble—Best of Family<br>(5 base models: 1 GBM, 1 XGBoost, 2 DRF, 1 DNN; metalearner: GLM, 5-fold CV)   | 41.24     | 35.59    | 27.41     | 18.71    | 162           |
| Ultralight    | VSC    | Stacked Ensemble—All Models<br>(8 of 20 base models: 3 GBM, 1 XGBoost, 1 DRF, 3 DNN; metalearner: GLM, 5-fold CV) | 1.41      | 1.08     | 1.39      | 1.11     | 158           |
| Standard Thin | IB     | Stacked Ensemble—All Models<br>(8 of 20 base models: 2 GBM, 2 XGBoost, 3 DNN, 1 DRF; metalearner: GLM, 5-fold CV) | 150.24    | 117.74   | 78.93     | 49.68    | 69            |
| Standard Thin | VSC    | Stacked Ensemble—Best of Family<br>(4 base models: 1 GBM, 1 XGBoost, 1 DNN, 1 GLM; metalearner: GLM, 5-fold CV)   | 2.13      | 1.60     | 1.78      | 1.31     | 67            |

Notes: Val. = validation subset. RMSE and MAE for IB are expressed in kPa; for VSC, in index units. Stacked Ensemble Best of Family combines the single best model from each algorithm family; Stacked Ensemble All Models draws from the full candidate pool. In both cases the metalearner was a GLM fitted on 5-fold cross-validated predictions from the base models. The number of base models actually used by the metalearner (selected column) may be smaller than the total trained, as the GLM regularization can assign zero weight to some candidates. Test metrics were computed after model selection was fixed and were not used to rank or replace candidates.

The larger errors obtained for Standard Thin panels indicate that the available DCS variables represented IB variation less effectively for this product family. This result is consistent with the sensitivity of thin panels to local variation in mat formation, moisture distribution, and press behavior, although the observational data do not permit a causal attribution of the error difference [7].

Figure 4 compares observed and predicted values for Ultralight panels across the three subsets. Predictions remain generally centered around the 1:1 line, while larger residuals occur mainly near the extremes of the observed range. Because the subsets were randomly sampled from the same production period, differences among them are interpreted as hold-out variation rather than as evidence of performance under future operating conditions.



**Figure 4.** Observed and predicted quality responses for Ultralight MDF. (a) Internal Bond strength and (b) Vertical Density Profile Index across the training, validation, and test subsets. The diagonal represents perfect agreement.

### 3.3.2. Vertical Density Profile Index Prediction Performance

For Ultralight panels, the selected VSC model achieved a validation RMSE of 1.41 and a test RMSE of 1.39. The corresponding MAE values were 1.08 and 1.11, respectively. For Standard Thin panels, validation and test RMSE were 2.13 and 1.78, while MAE was 1.60 and 1.31.

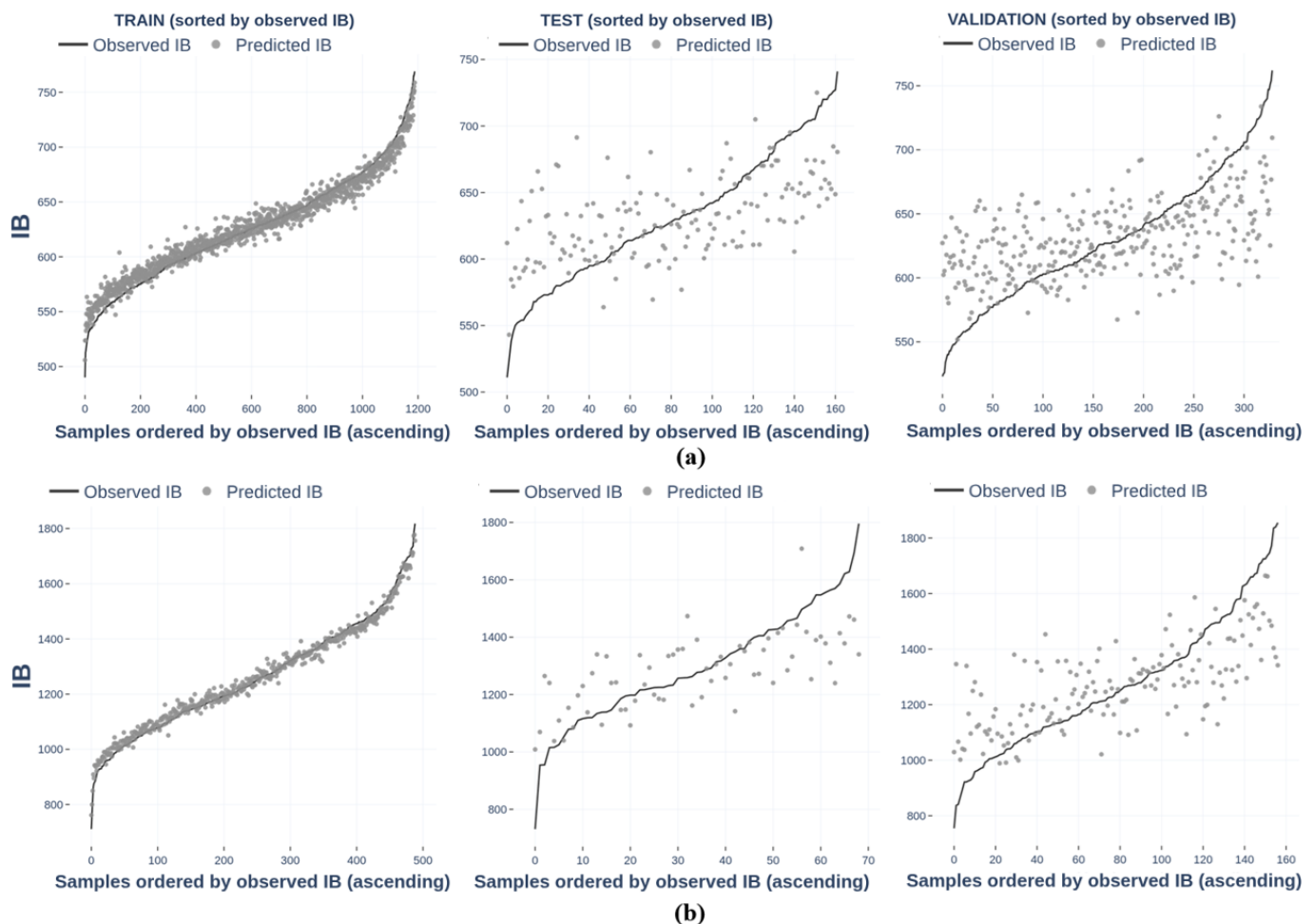
Because IB and VSC are reported on different scales, their absolute error values are not directly comparable. The similar validation and test errors observed for VSC indicate stable hold-out performance within the randomly partitioned production data. This result should not be interpreted as evidence of prospective performance on a later production period.

### 3.3.3. Observed and Predicted Trends Across the Response Range

Figure 5 compares observed and predicted IB values for Ultralight and Standard Thin panels across the three subsets, with samples ordered by observed IB. This representation shows how prediction fidelity changes across the response range.

For Ultralight panels, the predicted curve follows the observed pattern with moderate local deviations. For Standard Thin panels, the mismatch is more pronounced, particularly

where the observed response changes abruptly. This pattern is consistent with the larger errors reported in Table 7.



**Figure 5.** Observed and predicted Internal Bond strength for (a) Ultralight and (b) Standard Thin MDF across the training, validation, and test subsets. Samples are ordered by observed IB.

### 3.4. Error Structure and Relevance for Inspection Support

Aggregate regression metrics were complemented by graphical analysis of the error structure across the observed quality range. The parity and response-ordered plots show that prediction errors were distributed across the response range, although larger deviations occurred near some extreme observations.

For Ultralight IB, the mean percentage errors were 3.16%, 2.98%, and 2.82% in the low-, normal-, and high-quality bands, respectively. For Ultralight VSC, the corresponding values were 1.31%, 1.29%, and 1.26%. These results indicate that the average relative error did not concentrate strongly in one quality band.

The percentage-error analysis describes the distribution of continuous prediction errors, but it does not establish conformity-detection performance. As shown in Figure 3, the available IB observations were concentrated mainly above the operating quality ranges, particularly for Standard Thin panels. The number of observations near or below the lower acceptance limits was therefore insufficient for a stable estimation of sensitivity, specificity, precision, and false-negative rate.

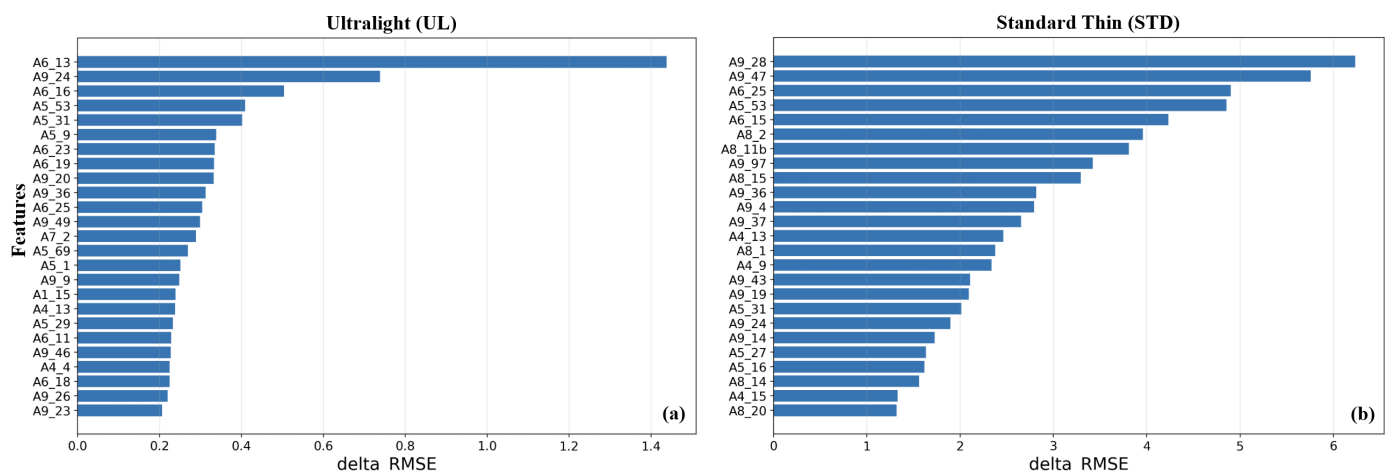
For this reason, no inspection-cost or sampling-reduction simulation was introduced. Such a simulation would require reliable estimates of the probability of missing non-conforming production, which cannot be obtained from a dataset dominated by acceptable

and over-quality observations. The present models should instead be interpreted as continuous monitoring tools that can identify deviations from the desired operating range, including persistent over-quality.

### 3.5. Process-Relevant Predictive Drivers

The selected model differed according to the product–target combination. Because the available global importance rankings were obtained from an individual GBM, they were used as an auxiliary analysis of predictive relevance within that learner. These rankings should not be interpreted as a direct explanation of the selected model when the final candidate corresponded to another algorithm or to a stacked ensemble.

Figure 6 presents the global feature-importance rankings for IB prediction in Ultralight and Standard Thin panels. In both cases, the leading tags are concentrated in areas associated with drying, resin and additive application, and hot pressing. These variables were informative within the GBM model and are physically consistent with known mechanisms related to moisture conditioning, dosing stability, and thermal-mechanical consolidation.



**Figure 6.** Global feature-importance rankings for Internal Bond prediction obtained from the strongest individual GBM evaluated during the AutoML search. (a) Ultralight MDF and (b) Standard Thin MDF. The rankings describe predictive relevance within the GBM and are presented as an auxiliary interpretation rather than as a direct explanation of every selected final model.

At the process level, the ranking pattern is consistent with the view that board quality develops through coupled interactions among moisture conditioning, resin application, and thermal-mechanical consolidation [7,24]. However, the reported importance values describe predictive relevance and should not be interpreted as causal effects.

A model-agnostic importance analysis applied directly to each selected model would be needed to determine whether the same ranking structure is retained across the complete predictive pipeline.

To assess whether this structure was retained in the final selected model, permutation feature importance (PFI) and SHAP values were calculated directly from the ensemble prediction function on the independent test set. For IB, the ensemble-level permutation analysis ranked A9\_24, A5\_1, A6\_55 and A6\_13 as the main predictors, with test-set RMSE increases of  $1.489 \pm 0.674$ ,  $1.424 \pm 0.444$ ,  $1.349 \pm 0.458$  and  $0.819 \pm 0.343$ , respectively. The model-agnostic SHAP analysis identified the same four variables as the dominant contributors. Ranking concordance across the training, validation and test partitions was moderate, with Kendall's  $W = 0.609$ . Despite variability among predictors with small importance, the four dominant variables remained within the first four positions in every partition.

For VSC, A9\_66 was consistently the leading predictor, followed by A6\_29 and A5\_57. Permuting A9\_66 increased test RMSE by  $0.168 \pm 0.017$ , equivalent to 11.57% of the baseline test RMSE. The PFI and SHAP rankings were strongly correlated for VSC, with Spearman's  $\rho = 0.765$ , and eight variables were shared by their respective top-10 sets. Ranking stability across data partitions was high, with Kendall's  $W = 0.861$  and pairwise Spearman correlations ranging from 0.744 to 0.843.

### 3.6. Inspection-Oriented Interpretation

The results show that industrial DCS data contain information that is useful for estimating IB and VSC before laboratory confirmation. Within the scope of the available data, the models are most appropriately viewed as continuous process-monitoring tools rather than as conformity classifiers.

For IB, the principal operational pattern was systematic over-quality. The central values of both product distributions exceeded their respective upper operating reference limits, with the largest deviation observed for Standard Thin panels. This result identifies a potential opportunity to reduce quality giveaway by adjusting resin dosage, thermal input, pressing conditions, or related operating variables while preserving the required IB level. Any such adjustment would require controlled industrial validation before implementation.

The current dataset does not support a reliable assessment of sensitivity, specificity, precision, false-negative rate, or inspection cost because near-threshold and non-conforming observations were poorly represented. Consequently, the models cannot yet be used to justify a reduction in destructive testing or to replace formal conformity assessment.

Their supported role is to provide an additional indication of process behavior, identify persistent departures from the desired quality range, and assist the review of operating periods associated with excessive or unstable quality. A prospective study containing sufficient observations near and below the acceptance thresholds is required to validate conformity detection, sampling-reduction strategies, and inspection-cost trade-offs.

## 4. Discussion

The results demonstrate that industrial DCS data can support inspection-oriented predictive quality modeling in continuous MDF manufacturing when the production line is treated as an integrated system of coupled subsystems rather than a collection of independent unit operations. The differential predictability of VSC and IB, the product-class-specific error structure, and the physical coherence of the feature-importance rankings collectively reflect the distributed nature of quality formation across the nine production stages analyzed in this study.

### 4.1. VSC Predictability and Its Physical Basis

Vertical Density Profile Index was predicted with lower error than Internal Bond across both product families, a result that is consistent with the physical mechanisms governing each response. VSC is closely linked to drying stability, resin and additive dosing, steam conditions, and thermal operating regimes process stages that are comparatively well instrumented in the studied DCS architecture. The most relevant predictors for VSC included variables from the dryer discharge moisture control (A6\_29), dryer differential pressure, steam pressure at the dryer inlet, and resin-line flow rates. These variables directly reflect the moisture removal and thermal history that govern density development through the panel thickness during drying and pressing. VSC is therefore tractable from routine sensor signals [7,24].

The close match between validation and test errors for the VSC-UL model (RMSE: 1.41 vs. 1.39; MAE: 1.08 vs. 1.11) indicates stable generalization, suggesting that the underlying process–quality relationship is sufficiently captured by the available DCS signals and that the temporal variability of those signals across the training period represents the range encountered at test time.

#### 4.2. IB Predictability and Emergent Mechanical Behavior

Internal Bond was harder to predict than VSC, especially for STD panels. IB is an emergent mechanical response that depends on fiber morphology, resin distribution, adhesive curing kinetics, heat and mass transfer during pressing, and vertical density profile development [14,36]. Several of these mechanisms are only indirectly observable through routine DCS tags: standard process historians do not record core-layer temperature evolution, fiber-level resin coverage, or cross-thickness density gradients. The model must therefore infer bonding quality from indirect proxies rather than from direct measurements of the mechanisms that determine IB.

This interpretive gap is more pronounced in STD panels, where reduced thickness increases sensitivity to localized disturbances in mat formation, moisture redistribution, and press closure dynamics. The larger errors for STD RMSE of 78.93 kPa versus 27.41 kPa for UL are consistent with findings in the broader MDF literature showing that thin boards have limited tolerance to local variations in mat distribution and compression history, and that small deviations in these stages produce disproportionately large changes in bonding performance [7,37].

The stronger IB performance for UL panels suggests that the available process tags provide a more stable representation of the mechanisms governing bonding behavior in that product family. The higher bulk-to-thickness ratio in UL panels reduces the relative influence of surface-layer and core-layer density gradients on measured IB, making the response less sensitive to localized press dynamics not captured by the historian. This structural argument is supported by the observation that the most relevant IB predictors for UL were concentrated in thermal conditioning, resin transport, and press cooling, which are more uniformly sensed along the continuous press than core-specific curing behavior.

#### 4.3. Feature Importance and the Systems-Oriented Interpretation

The global importance rankings are physically coherent across both product families and both quality targets. For UL panels, the most influential tags included variables associated with dust-to-process flow (A6\_13), press cooling temperature (A9\_24), dryer differential pressure (A6\_14–A6\_16), defibrator chamber pressure (A5\_52–A5\_53), blow-valve behavior (A5\_31), ECOR resin-line flow (A5\_2), dryer-inlet steam pressure (A6\_23–A6\_24), and press steam conditions (A9\_57). These variables link predictive performance to furnish flow stability, moisture removal, fiber transport, resin delivery, and thermal conditioning before final consolidation.

For STD panels, the highest-ranked variables were concentrated in hot-press heating circuits (A9\_26–A9\_43), compression circuits (A9\_45–A9\_49), dryer pressure behavior, defibrator pressure, mat humidification (A8\_1–A8\_2), and forming-head position (A8\_8–A8\_9). The prominence of heating-circuit temperature, compression-circuit response, press steam pressure, and forming-head outlet position is consistent with the greater sensitivity of thin boards to interactions between mat preparation and press thermodynamics, as identified in process-level studies of continuous flat-pressing systems [7,26].

These rankings are consistent with findings from large-scale data-driven analyses of MDF manufacturing, in which flash-tube dryer, mat forming, and hot-pressing variables were identified as the primary contributors to density and IB outcomes across thousands of production records [37]. The convergence of results across methodologies ensemble ML on DCS data in this study versus regularized regression on a much larger historian in the cited work reinforces the physical credibility of the importance structure reported here.

The importance rankings should nonetheless be interpreted as indicators of global predictive relevance within the fitted models, not as evidence of direct causality. Variables that appear highly ranked may reflect correlated operating regimes or shared control loops rather than independent physical mechanisms. The value of the rankings lies in directing process-engineering attention to the stages of the line that carry the most quality-relevant information under current instrumentation, not in establishing mechanistic pathways.

From a systems perspective, the recurrence of variables from drying, chemical defibration, forming, and pressing across both product families supports the core argument of this study: final MDF quality is not determined by any single control variable but by the combined effect of interconnected process subsystems distributed along the production line [7,8]. Moisture conditioning in A6–A7 affects resin cure kinetics and heat transfer in A9; resin and additive dosing in A5 influences bond formation during pressing; mat forming in A8 controls uniformity and basis weight, which determine compression response; pressing in A9 integrates all upstream variability into the final density and curing state. The stacked ensemble captures this distributed structure through nonlinear combinations of signals from multiple subsystems, which is precisely why ensemble methods outperformed single-stage models in all four prediction tasks.

#### *4.4. Operational Interpretation and Inspection Role*

From an industrial standpoint, the reported error levels indicate that the models are more suitable for inspection-oriented decision support than for replacing laboratory testing, consistent with the design intent stated in Section 2.8 [10,38]. Their operational value lies in reducing the delay between process drift and quality verification. For VSC, the relatively stable prediction errors across both product families suggest that the model can support near-real-time pre-screening as part of a broader quality-assurance workflow. For IB, the model should be applied with greater caution: UL panels can be screened with moderate confidence, while STD panels should be treated primarily as a risk-stratification context, flagging production intervals that warrant priority laboratory verification.

Deviations in variables related to dryer pressure, steam conditions, resin-line flow, forming-head position, humidification, press temperature, and compression response should be treated as process states with elevated relevance for quality monitoring. This operational logic connects the predictive model to the inspection planning cycle: when these variables signal atypical states, the probability of quality drift is higher, and targeted laboratory testing is likely to be more informative than uniform sampling [39,40].

The percentage-error stratification by quality band (Table 8) supports this interpretation. The balanced error distribution across low-, normal-, and over-quality regimes in UL panels indicates that the model does not systematically fail in any single quality region, which is a prerequisite for inspection use. A model that is accurate only in the normal-quality regime would provide no useful signal at the boundaries where intervention is most needed. The maximum error of 17.26% for IB-UL and 5.14% for VSC-UL defines the practical uncertainty envelope within which inspection decisions must be made.

**Table 8.** Performance summary for Ultralight MDF panels, including dataset sizes, validation and test errors, and percentage errors by quality band.

| Metric                         | Training | Validation | Testing |
|--------------------------------|----------|------------|---------|
| <b>IB—Ultralight</b>           |          |            |         |
| Observations                   | 1189     | 329        | 162     |
| Predictor variables            | 55       | 55         | 55      |
| RMSE (kPa)                     | —        | 41.24      | 27.41   |
| MAE (kPa)                      | —        | 35.59      | 18.71   |
| Mean error, low quality (%)    | —        | —          | 3.16    |
| Mean error, normal quality (%) | —        | —          | 2.98    |
| Mean error, high quality (%)   | —        | —          | 2.82    |
| Maximum error (%)              | —        | —          | 17.26   |
| <b>VSC—Ultralight</b>          |          |            |         |
| Observations                   | 1195     | 327        | 158     |
| Predictor variables            | 72       | 72         | 72      |
| RMSE (index)                   | —        | 1.41       | 1.39    |
| MAE (index)                    | —        | 1.08       | 1.11    |
| Mean error, low quality (%)    | —        | —          | 1.31    |
| Mean error, normal quality (%) | —        | —          | 1.29    |
| Mean error, high quality (%)   | —        | —          | 1.26    |
| Maximum error (%)              | —        | —          | 5.14    |

#### 4.5. Limitations and Directions for Future Work

Several limitations of the current framework should be acknowledged. First, the data originate from routine industrial operation, where laboratory measurements are sparse relative to DCS signal frequency. The imbalance between predictor density and response density constrains model complexity and limits the detection of short-term quality transients. Second, several physical mechanisms central to IB formation core-layer bonding, fiber-level resin distribution, and vertical density profile development are only indirectly represented by standard DCS instrumentation [14,36]. Third, stacked and ensemble-based models improve predictive performance but reduce direct mechanistic interpretability; the importance rankings provide directional guidance but do not quantify causal contributions.

Future work should address these limitations along three complementary directions. The first is richer process representation: incorporating inline measurements of mat moisture distribution, press-gap evolution, core-layer temperature, and density profile would provide more direct observability of the mechanisms that govern IB, particularly in thin boards. The second is temporal modeling: explicit residence-time alignment, process-lag estimation, and sequential modeling of the material trajectory through the production line could improve temporal consistency and reduce prediction error for responses that integrate upstream variability over extended time windows [24,31]. The third is physics-informed modeling: hybrid approaches that embed heat transfer, moisture migration, resin curing, or press consolidation knowledge directly into the model architecture could improve both accuracy and interpretability, particularly for IB prediction in thin MDF products where purely data-driven methods face fundamental observability limits [41].

## 5. Conclusions

This study developed and evaluated an inspection-oriented predictive quality framework for continuous MDF manufacturing using industrial Distributed Control System (DCS) data and automated machine learning. The framework was designed to operate as a decision-support component within a broader quality-assurance system, linking pro-

cess sensing, model-based interpretation, and inspection planning across a nine-stage production line treated as an integrated, coupled system.

The following conclusions are drawn from the experimental results:

1. **DCS data support useful quality estimates when the pipeline is carefully designed.** Process historian variables can provide reliable early estimates of selected quality attributes provided that preprocessing, collinearity control, target-specific feature selection, and product-family separation are applied systematically. The proposed pipeline RF-based imputation, Pearson collinearity filtering at  $|r| \geq 0.8$ , importance-based pruning, and H2O AutoML with stacked ensembles is transferable to other continuous wood-based panel lines with comparable DCS architectures.
2. **VSC is a robust target for near-real-time predictive monitoring.** Vertical Density Profile Index was the most consistently predicted quality variable across both Ultra-light (UL) and Standard Thin (STD) panels, with test RMSE of 1.39 and 1.78 (index units) respectively, and balanced percentage errors across quality bands. Its close connection to drying stability, steam pressure, thermal conditions, and resin dosing makes it directly traceable from routine sensor signals and a suitable candidate for operational deployment.
3. **IB prediction is feasible for UL panels but remains a risk-screening tool for STD panels.** Internal Bond was harder to predict, particularly for Standard Thin panels (test RMSE: 78.93 kPa vs. 27.41 kPa for UL), confirming that bonding strength is governed by mechanisms that are only indirectly observable through standard DCS instrumentation: fiber morphology, resin distribution, mat uniformity, moisture-dependent heat transfer, curing progression, and vertical density profile development [14,36]. For UL panels, the IB model provides sufficient accuracy for pre-screening. For STD panels, the model is best used to flag production intervals warranting priority laboratory verification rather than as a direct quality estimator.
4. **Feature importance rankings are physically coherent and process-stage-specific.** The most influential predictors for UL were concentrated in drying behavior, press cooling temperature, dryer pressure balance, resin-line flow, defibrator pressure, blow-valve behavior, and steam conditions. For STD panels, the dominant predictors shifted toward press heating circuits, compression circuits, dryer differential pressure, mat humidification, and forming-head position. These patterns are consistent with large-scale data-driven analyses of MDF manufacturing [37], and confirm that predictive performance arises from the interaction of multiple process stages rather than from any single sensor signal.
5. **A systems perspective is necessary and sufficient for framing MDF quality prediction.** Final board quality is not determined by isolated control variables but by the coupled effect of interconnected subsystems spanning fiber preparation, chemical application, drying, forming, and hot pressing [7,8]. Treating the production line as an integrated system rather than a collection of independent unit operations is a methodological prerequisite. It also explains why the importance rankings and error patterns differ between product families in the way they do.
6. **The models function best as an inspection-support layer, not as a compliance substitute.** Operationally, the framework identifies production intervals with elevated quality risk, prioritizes destructive sampling, and reduces the delay between process drift and laboratory confirmation [10,38]. Formal laboratory testing remains the basis for compliance decisions; the predictive layer improves the responsiveness and targeting of that testing without replacing it.

Future work should address three limitations identified in this study. First, richer process representation including inline measurements of mat moisture distribution, press-

gap evolution, core-layer temperature, and vertical density profile would improve IB prediction in thin panels by providing direct observability of the mechanisms currently inferred from indirect proxies. Second, explicit temporal modeling through residence-time alignment and process-lag estimation would improve prediction consistency across production regimes and reduce sensitivity to batch-timestamp approximations [31]. Third, physics-informed hybrid modeling approaches that embed heat-transfer, resin-curing, or press-consolidation knowledge into the learning architecture could improve both accuracy and interpretability for responses that depend on mechanisms not directly sensed by routine DCS instrumentation [41].

Collectively, these advances would support broader deployment of predictive quality frameworks in continuous wood-based panel manufacturing as components of Industry 4.0 cyber-physical production systems, where process sensing, model-based interpretation, and inspection planning are integrated into a unified, adaptive quality-assurance architecture [8,40].

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## Abbreviations

The following abbreviations are used in this manuscript:

|        |                                |
|--------|--------------------------------|
| AI     | Artificial Intelligence        |
| ANN    | Artificial Neural Network      |
| AutoML | Automated Machine Learning     |
| CARB   | California Air Resources Board |
| DCS    | Distributed Control System     |
| GBM    | Gradient Boosting Machine      |
| GLM    | Generalized Linear Model       |

|      |                                |
|------|--------------------------------|
| IB   | Internal Bond strength         |
| MAE  | Mean Absolute Error            |
| MDF  | Medium-Density Fiberboard      |
| ML   | Machine Learning               |
| MOE  | Modulus of Elasticity          |
| MOR  | Modulus of Rupture             |
| PLC  | Programmable Logic Controller  |
| PQ   | Predictive Quality             |
| RF   | Random Forest                  |
| RMSE | Root Mean Squared Error        |
| STD  | Standard Thin MDF panels       |
| UL   | Ultralight MDF panels          |
| UF   | Urea–Formaldehyde resin        |
| VSC  | Vertical Density Profile Index |

## Appendix A

Appendix A provides the dictionary of process variables used in this study. The variables correspond to DCS tags collected from equipment and sensors distributed across the MDF production line, covering the main operational stages: wood preparation, fiber preparation, defibration, chemical application, drying, forming, and hot pressing. For each process tag, the dictionary reports the original plant identifier, a descriptive label, and the coded variable name used during preprocessing, feature selection, and model development. This structure ensures traceability between the industrial historian records and the machine-learning predictors, while also supporting process-level interpretation of the models. The recorded variables describe key operating conditions such as flow rates, pressures, temperatures, humidity, resin and additive dosing, mat properties, press settings, and compression-related signals, which together represent the observable state of the continuous MDF manufacturing system.

**Table A1.** Dictionary of process tags and variables used in the study.

| Tag                   | Description                                    | Variable |
|-----------------------|------------------------------------------------|----------|
| E_677FI6726_PV        | Effluent inlet flow                            | A1_1     |
| E_ES0201_PV           | Dry chip reclaimer levelling roll load control | A1_2     |
| E_ES0221_PV           | Levelling roll load control                    | A1_3     |
| E_M0201M01EI_PV       | Fresh chip reclaimer screw current             | A1_4     |
| E_M0201M01RPM_PV      | Fresh chip reclaimer screw speed               | A1_5     |
| E_M0201M02EI_PV       | Fresh chip reclaimer slewing current           | A1_6     |
| E_M0201M02SI_PV       | Fresh chip reclaimer slewing speed             | A1_7     |
| E_M0202M09RPM_PV      | Dry chip reclaimer metering screw speed        | A1_8     |
| E_RSIC0200_PV         | Fresh chip reclaimer speed control             | A1_9     |
| E_RSIC0230_PV         | Dry chip metering screw speed control          | A1_10    |
| E_SIC0233_PV          | Sawdust silo discharge No. 1 speed control     | A1_11    |
| E_WI0206_PV           | Fresh chip flow indication                     | A1_12    |
| E_WI0207_PV           | Dry chip flow indication                       | A1_13    |
| H_EI_52_21_PV         | General 220 kV line power (breaker 52-21)      | A1_14    |
| H_PIA0280_PV          | Industrial water network pressure              | A1_15    |
| H_PIA0281_PV          | Air network pressure                           | A1_16    |
| P_EI_SUBESTAC2_BAT_PV | MDF2 substation No. 2 battery bank voltage     | A1_17    |
| E_LC0202_PV           | Chip wash circulation tank level control       | A2_1     |
| E_LIA0232_PV          | Sawdust silo level indication and alarm        | A2_2     |
| E_LIC0225_PV          | Sawdust (PRS) metering bin level control       | A2_3     |

Table A1. Cont.

| Tag                    | Description                                               | Variable |
|------------------------|-----------------------------------------------------------|----------|
| E_LIC0232_PV           | Sawdust silo level indication                             | A2_4     |
| E_M0237M010203RPM_PV   | Sawdust metering bin screws No. 1, No. 2 and No. 3 speed  | A2_5     |
| E_M0237M010203SI_PV    | Sawdust metering bin screws No. 1, No. 2 and No. 3 speed  | A2_6     |
| E_M0238M01RPM_PV       | Sawdust weigh-scale conveyor speed                        | A2_7     |
| E_M0250M02RPM_PV       | Sawdust silo outfeed screw No. 1 speed                    | A2_8     |
| E_M0250M02SI_PV        | Sawdust silo outfeed screw No. 1 speed                    | A2_9     |
| E_M0250M03RPM_PV       | Sawdust silo outfeed screw No. 2 speed                    | A2_10    |
| E_M0250M03SI_PV        | Sawdust silo outfeed screw No. 2 speed                    | A2_11    |
| E_M0257_IIC_01_PV      | Robox current                                             | A2_12    |
| E_PIA0242_PV           | Sawdust blower line No. 1 pressure                        | A2_13    |
| E_PIA0243_PV           | Sawdust blower line No. 2 pressure                        | A2_14    |
| E_RWIC0226_PV          | Sawdust flow control                                      | A2_15    |
| E_SICM0221_03_PV       | Sawdust silo A screw speed control                        | A2_16    |
| E_SICM0221_04_PV       | Sawdust silo B screw speed control                        | A2_17    |
| E_SICM0237_01_02_PV    | Sawdust metering bin screws No. 1 and No. 2 speed control | A2_18    |
| E_SICM0238_01_PV       | Sawdust weigh conveyor speed control                      | A2_19    |
| P_AIC003_PV            | Clean water tank pH                                       | A2_20    |
| P_FIC008_PV            | Clean water pump flow                                     | A2_21    |
| H_FIC0336_PV           | Mixing screw steam flow                                   | A3_1     |
| H_LICA0300_PV          | Steaming bin level control                                | A3_2     |
| H_LICA0304_PV          | Sawdust metering bin level control                        | A3_3     |
| H_M0301M01SI_PV        | Steaming bin discharge screw No. 1 speed                  | A3_4     |
| H_M0301M03SI_PV        | Steaming bin discharge screw No. 3 speed                  | A3_5     |
| H_M0301M05SI_PV        | Steaming bin discharge screw No. 5 speed                  | A3_6     |
| H_M0302M01SI_PV        | Sawdust metering bin screw No. 1 speed                    | A3_7     |
| H_M0302M03SI_PV        | Sawdust metering bin screw No. 3 speed                    | A3_8     |
| H_M0303M01SI_PV        | Mixing screw conveyor speed                               | A3_9     |
| H_WI0385_PV            | Sawdust flow (t/h)                                        | A3_10    |
| H_EI0322_PV            | Plug feed screw current                                   | A4_1     |
| H_EI0324_PV            | Preheater discharge screw current                         | A4_2     |
| H_FI0310_PV            | Preheater steam flow                                      | A4_3     |
| H_FI0326_PV            | Total 6 bar steam flow                                    | A4_4     |
| H_FI0380_PV            | Total 12.5 bar steam flow                                 | A4_5     |
| H_GHIC0308_PV          | Preheater hoist position and RTC                          | A4_6     |
| H_LC0342_PV            | Drain tank level                                          | A4_7     |
| H_LICA0303_PV          | ADI inlet chute level control                             | A4_8     |
| H_LICA0307_PV          | Preheater level control                                   | A4_9     |
| H_PIC0309_PV           | Preheater steam pressure                                  | A4_10    |
| H_SI0321_PV            | Plug feed screw speed                                     | A4_11    |
| H_TI0332_PV            | Preheater average temperature                             | A4_12    |
| H_TI0333_PV            | Plug feed screw flush water temperature                   | A4_13    |
| H_WI0335_PV            | Preheater discharge screw flow 324                        | A4_14    |
| PI_306_PV              | PI_306 cone valve pressure                                | A4_15    |
| H_WI0335_PV2           | Preheater discharge screw flow 335                        | A4_14b   |
| H_DPIC0311_PV          | Defibrator differential pressure                          | A5_1     |
| H_ECOR_GLINEFLOWSUM_PV | ECOR resin lines actual flow sum                          | A5_2     |
| H_ECOR_L1_FLOW_PV      | ECOR line 1 flow variable                                 | A5_3     |
| H_ECOR_L1_POS_PV       | ECOR line 1 position variable                             | A5_4     |
| H_ECOR_L10_FLOW_PV     | ECOR line 10 flow variable                                | A5_5     |
| H_ECOR_L10_POS_PV      | ECOR line 10 position variable                            | A5_6     |
| H_ECOR_L2_FLOW_PV      | ECOR line 2 flow variable                                 | A5_7     |
| H_ECOR_L2_POS_PV       | ECOR line 2 position variable                             | A5_8     |
| H_ECOR_L3_FLOW_PV      | ECOR line 3 flow variable                                 | A5_9     |
| H_ECOR_L3_POS_PV       | ECOR line 3 position variable                             | A5_10    |
| H_ECOR_L4_FLOW_PV      | ECOR line 4 flow variable                                 | A5_11    |

Table A1. Cont.

| Tag                     | Description                              | Variable |
|-------------------------|------------------------------------------|----------|
| H_ECOR_L4_POS_PV        | ECOR line 4 position variable            | A5_12    |
| H_ECOR_L5_FLOW_PV       | ECOR line 5 flow variable                | A5_13    |
| H_ECOR_L5_POS_PV        | ECOR line 5 position variable            | A5_14    |
| H_ECOR_L6_FLOW_PV       | ECOR line 6 flow variable                | A5_15    |
| H_ECOR_L6_POS_PV        | ECOR line 6 position variable            | A5_16    |
| H_ECOR_L7_FLOW_PV       | ECOR line 7 flow variable                | A5_17    |
| H_ECOR_L7_POS_PV        | ECOR line 7 position variable            | A5_18    |
| H_ECOR_L8_FLOW_PV       | ECOR line 8 flow variable                | A5_19    |
| H_ECOR_L8_POS_PV        | ECOR line 8 position variable            | A5_20    |
| H_ECOR_L9_FLOW_PV       | ECOR line 9 flow variable                | A5_21    |
| H_ECOR_L9_POS_PV        | ECOR line 9 position variable            | A5_22    |
| H_ECOR_STEAMPRESSURE_PV | ECOR steam pressure                      | A5_23    |
| H_EI0325_PV             | Defibrator feeder current                | A5_24    |
| H_EIC0368_PV            | Main motor power and SEC                 | A5_25    |
| H_FI0312_PV             | Defibrator steam flow                    | A5_26    |
| H_FI0487_PV             | ECOR steam flow                          | A5_27    |
| H_FIA0328_PV            | Defibrator mechanical seal steam flow    | A5_28    |
| H_GI0346_PV             | Defibrator rotor position                | A5_29    |
| H_GIA0360_PV            | Defibrator touchpoint vibration detector | A5_30    |
| H_HIC0314_PV            | Blow valve                               | A5_31    |
| H_LIA_0483_PV           | Resin tank 2 level indication            | A5_32    |
| H_LIA_0485_PV           | Resin tank 3 level indication            | A5_33    |
| H_LIA0440_PV            | Emulsion tank No. 1 level                | A5_34    |
| H_LIA0441_PV            | Emulsion tank No. 2 level                | A5_35    |
| H_LIA0481_PV            | Raw resin tank 1 level                   | A5_36    |
| H_LIA0483_PV            | Raw resin tank 2 level                   | A5_37    |
| H_LIA0485_PV            | Raw resin tank 3 level                   | A5_38    |
| H_LIC0412_PV            | Prepared resin level                     | A5_39    |
| H_LICA0449_PV           | Prepared scavenger level                 | A5_40    |
| H_M0402M01SI_PV         | Resin transfer pump No. 1 speed          | A5_41    |
| H_M0402M02SI_PV         | Resin transfer pump No. 2 speed          | A5_42    |
| H_M0402M05SI_PV         | Resin dosing pump No. 1 speed            | A5_43    |
| H_M0402M06SI_PV         | Resin dosing pump No. 2 speed            | A5_44    |
| H_M0402M10SI_PV         | Fungicide metering pump speed            | A5_45    |
| H_M0403M03SI_PV         | Hardener metering pump speed             | A5_46    |
| H_M0404M03SI_PV         | Scavenger metering pump speed            | A5_47    |
| H_M0407M01SI_PV         | Melted wax metering pump No. 1 speed     | A5_48    |
| H_M0407M02SI_PV         | Melted wax metering pump No. 2 speed     | A5_49    |
| H_M0408M01SI_PV         | Emulsion pump No. 1 speed                | A5_50    |
| H_M0408M03SI_PV         | Emulsion pump No. 3 speed                | A5_51    |
| H_PI0345_B_PV           | Defibrator B chamber pressure            | A5_52    |
| H_PI0345_PV             | Defibrator A chamber pressure            | A5_53    |
| H_PIA0486_PV            | Ecoresinator line pressure               | A5_54    |
| H_PIC0421_PV            | Wax steam pressure                       | A5_55    |
| H_R_390_PV              | Steam t/h to fiber t/h ratio             | A5_56    |
| H_RFIC0401_1_PV         | Melted wax pump No. 1 flow               | A5_57    |
| H_RFIC0401_2_PV         | Melted wax pump No. 2 flow               | A5_58    |
| H_RFIC0404_PV           | Raw resin flow No. 1                     | A5_59    |
| H_RFIC0405_PV           | Raw resin flow No. 2                     | A5_60    |
| H_RFIC0408_PV           | Prepared resin flow                      | A5_61    |
| H_RFIC0409_PV           | Scavenger flow                           | A5_62    |
| H_RFIC0414_PV           | Dilution water flow                      | A5_63    |
| H_RFICA0407_PV          | Hardener flow                            | A5_64    |
| H_RFICA0433_PV          | Emulsion flow                            | A5_65    |
| H_TIC0466_PV            | Wax feeding line No. 1 temperature       | A5_66    |

Table A1. Cont.

| Tag                 | Description                                                 | Variable |
|---------------------|-------------------------------------------------------------|----------|
| H_TIC0467_PV        | Wax feeding line No. 2 temperature                          | A5_67    |
| H_TIC0468_PV        | Wax return line temperature                                 | A5_68    |
| H_XIA0344_PV        | Defibrator vibration detector                               | A5_69    |
| O_EIC0368_PV        | Main motor power and SEC (filtered)                         | A5_70    |
| E_PIA0224_PV        | 15 bar steam pressure from boiler                           | A6_2     |
| E_PIA0250_PV        | 36 bar steam pressure from boiler, process value            | A6_3     |
| E_PIA0252_PV        | 4.5 bar steam pressure from boiler                          | A6_4     |
| H_DPI_504_PV        | Boiler silo dust filter differential pressure               | A6_5     |
| H_FI_15BAR_PV       | 15 bar steam flow from boiler                               | A6_6     |
| H_FI_4BAR_PV        | 4.5 bar steam flow from boiler                              | A6_7     |
| H_LICA0107_PV       | Condensate return level control                             | A6_8     |
| H_LICA0107B_PV      | Condensate return level control                             | A6_9     |
| H_TIA0225_PV        | 14 bar steam line temperature                               | A6_10    |
| H_TIA0251_PV        | 36 bar steam temperature from boiler                        | A6_11    |
| H_TIA0253_PV        | 4.5 bar steam temperature from boiler                       | A6_12    |
| H_WI0386_PV         | Dust-to-process flow (t/h)                                  | A6_13    |
| J_DP1A_501A_PV      | Dryer zone 1–2 differential pressure                        | A6_14    |
| J_DP1A_501B_PV      | Dryer zone 3–4 differential pressure                        | A6_15    |
| J_DP1A_501C_PV      | Dryer zone 5–6 differential pressure                        | A6_16    |
| J_FICA0501_PV       | Dryer inlet airflow control                                 | A6_17    |
| IO705_PV            | Fiber conditioning transport air inlet humidity             | A6_18    |
| J_MI0705B_PV        | Fiber conditioning transport air inlet temperature          | A6_19    |
| J_PI0550_PV         | Press flash steam tank pressure 50                          | A6_20    |
| J_PI0551_PV         | Press flash steam tank pressure 51                          | A6_21    |
| J_PI0552_PV         | Press flash steam tank pressure 52                          | A6_22    |
| J_PIA0526_PV        | 4.5 bar steam pressure at dryer inlet                       | A6_23    |
| J_PIA0527_PV        | 15 bar steam pressure at dryer inlet                        | A6_24    |
| J_PIA0550_PV        | Press steam tank pressure                                   | A6_25    |
| J_PIA0551_PV        | Flash steam tank pressure                                   | A6_26    |
| J_PIC0514_PV        | Dryer LP steam pressure                                     | A6_27    |
| J_PIC0518_PV        | Dryer HP steam pressure                                     | A6_28    |
| J_RMIC0505_PV       | Dryer discharge moisture indication and control             | A6_29    |
| J_RTICA0502_PV      | Dryer inlet air temperature control                         | A6_30    |
| J_RTICA0502_TE01_PV | Dryer inlet air temperature control                         | A6_31    |
| J_RTICA0502_TE02_PV | Dryer inlet air temperature control                         | A6_32    |
| J_RTICA0502_TE03_PV | Dryer inlet air temperature control                         | A6_33    |
| J_RTICA0502_TE04_PV | Dryer inlet air temperature control                         | A6_34    |
| J_RTICA0503_PV      | Dryer outlet air temperature control                        | A6_35    |
| J_RTICA0503_TE01_PV | Dryer outlet air temperature control                        | A6_36    |
| J_RTICA0503_TE02_PV | Dryer outlet air temperature control                        | A6_37    |
| J_SIC0509_PV        | Dryer discharge conveyor speed control                      | A6_38    |
| J_TIA0524_01_PV     | 4.5 bar steam temperature at dryer inlet                    | A6_39    |
| J_TIA0524_02_PV     | 4.5 bar steam temperature at dryer outlet                   | A6_40    |
| J_TIA0525_01_PV     | 15 bar steam temperature at dryer inlet                     | A6_41    |
| J_TIA0525_02_PV     | 15 bar steam temperature at dryer outlet                    | A6_42    |
| J_TIC0703_PV        | Fiber conditioning system heat exchanger outlet temperature | A6_43    |
| J_TICA0520_PV       | Dryer discharge conveyor temperature No. 1                  | A6_44    |
| J_TICA0520_TE02_PV  | Dryer discharge conveyor temperature No. 2                  | A6_45    |
| J_TICA0520_TE03_PV  | Dryer discharge conveyor temperature No. 3                  | A6_46    |
| J_TICA0520_TE04_PV  | Dryer discharge conveyor temperature No. 4                  | A6_47    |
| J_TICA0520_TE05_PV  | Dryer discharge conveyor temperature No. 5                  | A6_48    |
| J_TICA0520_TE06_PV  | Dryer discharge conveyor temperature No. 6                  | A6_49    |
| J_TICA0520_TE07_PV  | Dryer discharge conveyor temperature No. 7                  | A6_50    |
| J_TICA0520_TE08_PV  | Dryer discharge conveyor temperature No. 8                  | A6_51    |
| J_TICA0520_TE09_PV  | Dryer discharge conveyor temperature No. 9                  | A6_52    |

Table A1. Cont.

| Tag                              | Description                                       | Variable |
|----------------------------------|---------------------------------------------------|----------|
| J_TICA0520_TE10_PV               | Dryer discharge conveyor temperature No. 10       | A6_53    |
| J_TICA0520_TE11_PV               | Dryer discharge conveyor temperature No. 11       | A6_54    |
| J_XIA0517_PV                     | Dryer fan vibration indication                    | A6_55    |
| D_WI031_TACTUAL_PV               | 31E1 dust weight to process                       | A6_1b    |
| J_FIC0702_PV                     | Z-sifter recirculation airflow control            | A7_1     |
| J_PICA0701_PV                    | Z-sifter air pressure control                     | A7_2     |
| J_FIC0737A_PV                    | FIC_0737A lower IMAL humidifier flow              | A8_1     |
| J_FIC0837A_PV                    | FIC_0837A upper IMAL humidifier flow              | A8_2     |
| J_LIC0530_PV                     | Mat former level                                  | A8_3     |
| L_BOARD_TEMP_PV                  | Mat temperature                                   | A8_4     |
| L_DIA0804_PV                     | Mat density gauge indication                      | A8_5     |
| L_GIC0722_GE02_PV                | Forming head inlet position, right                | A8_6     |
| L_GIC0722_PV                     | Forming head inlet position, left                 | A8_7     |
| L_GIC0723_GT01_PV                | Forming head outlet position, right               | A8_8     |
| L_GIC0723_GT02_PV                | Forming head outlet position control              | A8_9     |
| L_GIC0723_GT02_PV2               | Forming head outlet position control              | A8_10    |
| L_M0801M01SI_PV                  | Precompressor upper drive                         | A8_12    |
| L_M0823M01SI_PV                  | Press infeed conveyor                             | A8_13    |
| L_MIC0730_PV                     | Forming conveyor moisture indication and control  | A8_14    |
| L_SIC0712_PV                     | Dosing bin bottom belt conveyor speed control     | A8_15    |
| L_SIC0726_PV                     | Forming conveyor speed control                    | A8_16    |
| L_TI0835_PV                      | Fiber mat temperature                             | A8_17    |
| L_WIC0728_PV                     | Forming conveyor mat weigh-scale weight control   | A8_18    |
| O_FORMING_MAT_DENSITY_PV         | Forming mat density                               | A8_19    |
| O_FORMING_MAT_HEIGHT_PV          | Forming mat height (measured)                     | A8_20    |
| O_FORMING_MAT_WEIGHT_PV          | Forming mat weight                                | A8_21    |
| L_LIA0710_PV2                    | Dosing bin level indication                       | A8_11b   |
| L_MIC0730_PV                     | Forming conveyor moisture indication and control  | A8_14c   |
| L_WIC0728_PV                     | Forming conveyor mat weigh-scale weight control   | A8_18c   |
| ACTADDWIDTHADJ                   | Width adjustment                                  | A9_1     |
| ACTDRVCURRENTMAINDRVBOT          | Main drive bottom current                         | A9_2     |
| ACTDRVCURRENTMAINDRVTOP          | Main drive top current                            | A9_3     |
| ACTDRVPOWERMAINDRVBOT            | Main drive bottom power consumption               | A9_4     |
| ACTDRVPOWERMAINDRVTOP            | Main drive top power consumption                  | A9_5     |
| ACTDRVSPEEDBOT                   | Bottom speed                                      | A9_6     |
| ACTDRVSPEEDTOP                   | Top speed                                         | A9_7     |
| ACTFBCTRLROLLCENTERBOTINMM       | Center control roll bottom position (mm)          | A9_8     |
| ACTFBCTRLROLLCENTERTOPINMM       | Center control roll top position (mm)             | A9_9     |
| ACTFBCTRLROLLINFEEDBOTINMM       | Infeed control roll bottom position (mm)          | A9_10    |
| ACTFBCTRLROLLINFEEDTOPINMM       | Infeed control roll top position (mm)             | A9_11    |
| ACTFBDRUMPOSINFEEDBOTINMM        | Infeed drum bottom position (mm)                  | A9_12    |
| ACTFBDRUMPOSINFEEDTOPINMM        | Infeed drum top position (mm)                     | A9_13    |
| ACTFBDRUMPOSOUTFEEDBOTLEFT       | Outfeed drum bottom-left position                 | A9_14    |
| ACTFBDRUMPOSOUTFEEDBOTRIGHT      | Outfeed drum bottom-right position                | A9_15    |
| ACTFBDRUMPOSOUTFEEDTOLEFT        | Outfeed drum top-left position                    | A9_16    |
| ACTFBDRUMPOSOUTFEEDTOPRIGHT      | Outfeed drum top-right position                   | A9_17    |
| ACTFBINFEEDADJLEFT               | Infeed adjustment, left side (upper drum height)  | A9_18    |
| ACTFBINFEEDADJRIGHT              | Infeed adjustment, right side (upper drum height) | A9_19    |
| ACTFBTRACKINGPRESSUREBOTLEFTBAR  | Bottom-left tracking pressure (bar)               | A9_20    |
| ACTFBTRACKINGPRESSUREBOTRIGHTBAR | Bottom-right tracking pressure (bar)              | A9_21    |
| ACTFBTRACKINGPRESSURETOLEFTBAR   | Top-left tracking pressure (bar)                  | A9_22    |
| ACTFBTRACKINGPRESSURETOPRIGHTBAR | Top-right tracking pressure (bar)                 | A9_23    |
| ACTHTTEMPCOOLINGAREAINFEED       | Cooling area inlet temperature                    | A9_24    |
| ACTHTTEMPCOOLINGAREAOUTFEED      | Cooling area outlet temperature                   | A9_25    |
| ACTHTTEMPHEATINGCIRCUIT1BOT      | Heating circuit 1 bottom temperature              | A9_26    |

Table A1. Cont.

| Tag                          | Description                                | Variable |
|------------------------------|--------------------------------------------|----------|
| ACTHTTEMPHEATINGCIRCUIT1FEED | Heating circuit 1 feeding-pipe temperature | A9_27    |
| ACTHTTEMPHEATINGCIRCUIT1TOP  | Heating circuit 1 top temperature          | A9_28    |
| ACTHTTEMPHEATINGCIRCUIT2BOT  | Heating circuit 2 bottom temperature       | A9_29    |
| ACTHTTEMPHEATINGCIRCUIT2FEED | Heating circuit 2 feeding-pipe temperature | A9_30    |
| ACTHTTEMPHEATINGCIRCUIT2TOP  | Heating circuit 2 top temperature          | A9_31    |
| ACTHTTEMPHEATINGCIRCUIT3BOT  | Heating circuit 3 bottom temperature       | A9_32    |
| ACTHTTEMPHEATINGCIRCUIT3FEED | Heating circuit 3 feeding-pipe temperature | A9_33    |
| ACTHTTEMPHEATINGCIRCUIT3TOP  | Heating circuit 3 top temperature          | A9_34    |
| ACTHTTEMPHEATINGCIRCUIT4BOT  | Heating circuit 4 bottom temperature       | A9_35    |
| ACTHTTEMPHEATINGCIRCUIT4FEED | Heating circuit 4 feeding-pipe temperature | A9_36    |
| ACTHTTEMPHEATINGCIRCUIT4TOP  | Heating circuit 4 top temperature          | A9_37    |
| ACTHTTEMPHEATINGCIRCUIT5BOT  | Heating circuit 5 bottom temperature       | A9_38    |
| ACTHTTEMPHEATINGCIRCUIT5FEED | Heating circuit 5 feeding-pipe temperature | A9_39    |
| ACTHTTEMPHEATINGCIRCUIT5TOP  | Heating circuit 5 top temperature          | A9_40    |
| ACTHTTEMPHEATINGCIRCUIT6BOT  | Heating circuit 6 bottom temperature       | A9_41    |
| ACTHTTEMPHEATINGCIRCUIT6FEED | Heating circuit 6 feeding-pipe temperature | A9_42    |
| ACTHTTEMPHEATINGCIRCUIT6TOP  | Heating circuit 6 top temperature          | A9_43    |
| ACTHTTEMPPRESSUREPOTCOOL     | Pressure pot cooling temperature           | A9_44    |
| ACTPRDCOMPRESSIONCIRCUIT01   | Actual compression circuit 1               | A9_45    |
| ACTPRDCOMPRESSIONCIRCUIT02   | Actual compression circuit 2               | A9_46    |
| ACTPRDCOMPRESSIONCIRCUIT03   | Actual compression circuit 3               | A9_47    |
| ACTPRDCOMPRESSIONCIRCUIT04   | Actual compression circuit 4               | A9_48    |
| ACTPRDCOMPRESSIONCIRCUIT05   | Actual compression circuit 5               | A9_49    |
| ACTPRDEGEIOILPRESSUREC1      | Actual edge oil pressure, circuit No. 1    | A9_50    |
| ACTPRDEGEIOILPRESSUREC2      | Actual edge oil pressure, circuit No. 2    | A9_51    |
| ACTPRDEGEIOILPRESSUREC3      | Actual edge oil pressure, circuit No. 3    | A9_52    |
| ACTPRDEGEIOILPRESSUREC4      | Actual edge oil pressure, circuit No. 4    | A9_53    |
| ACTPRDHUMIDITY               | Humidity                                   | A9_54    |
| ACTPRDWEIGHT                 | Product weight                             | A9_55    |
| ACTSTEAMFLOW                 | Actual 36 bar steam flow                   | A9_56    |
| ACTSTEAMPRESSURE             | Actual 36 bar steam pressure               | A9_57    |
| ACTSTEAMTEMPERATURE          | Actual 36 bar steam temperature            | A9_58    |
| CALAUTO_ENCODER_01R          | CALAUTO encoder 01R                        | A9_59    |
| CALAUTO_ENCODER_03R          | CALAUTO encoder 03R                        | A9_60    |
| CALAUTO_ENCODER_05R          | CALAUTO encoder 05R                        | A9_61    |
| CALAUTO_ENCODER_07R          | CALAUTO encoder 07R                        | A9_62    |
| CALAUTO_ENCODER_09R          | CALAUTO encoder 09R                        | A9_63    |
| CALAUTO_ENCODER_11R          | CALAUTO encoder 11R                        | A9_64    |
| CALAUTO_ENCODER_13R          | CALAUTO encoder 13R                        | A9_65    |
| CALAUTO_ENCODER_15R          | CALAUTO encoder 15R                        | A9_66    |
| CALAUTO_ENCODER_17R          | CALAUTO encoder 17R                        | A9_67    |
| CALAUTO_ENCODER_19R          | CALAUTO encoder 19R                        | A9_68    |
| CALAUTO_ENCODER_20L          | CALAUTO encoder 20L                        | A9_69    |
| CALAUTO_ENCODER_21R          | CALAUTO encoder 21R                        | A9_70    |
| CALAUTO_ENCODER_22L          | CALAUTO encoder 22L                        | A9_71    |
| CALAUTO_ENCODER_23R          | CALAUTO encoder 23R                        | A9_72    |
| CALAUTO_ENCODER_24L          | CALAUTO encoder 24L                        | A9_73    |
| CALAUTO_ENCODER_25R          | CALAUTO encoder 25R                        | A9_74    |
| CALAUTO_ENCODER_26L          | CALAUTO encoder 26L                        | A9_75    |
| CALAUTO_ENCODER_27R          | CALAUTO encoder 27R                        | A9_76    |
| CALAUTO_ENCODER_28L          | CALAUTO encoder 28L                        | A9_77    |
| CALAUTO_ENCODER_29R          | CALAUTO encoder 29R                        | A9_78    |
| CALAUTO_ENCODER_30L          | CALAUTO encoder 30L                        | A9_79    |
| CALAUTO_ENCODER_31R          | CALAUTO encoder 31R                        | A9_80    |
| CALAUTO_ENCODER_32L          | CALAUTO encoder 32L                        | A9_81    |

Table A1. Cont.

| Tag                        | Description                               | Variable |
|----------------------------|-------------------------------------------|----------|
| CALAUTO_ENCODER_33L        | CALAUTO encoder 33L                       | A9_82    |
| CALAUTO_ENCODER_33R        | CALAUTO encoder 33R                       | A9_83    |
| CALAUTO_ENCODER_35L        | CALAUTO encoder 35L                       | A9_84    |
| CALAUTO_ENCODER_37L        | CALAUTO encoder 37L                       | A9_85    |
| CALAUTO_ENCODER_37R        | CALAUTO encoder 37R                       | A9_86    |
| CALAUTO_ENCODER_40L        | CALAUTO encoder 40L                       | A9_87    |
| CALAUTO_ENCODER_40R        | CALAUTO encoder 40R                       | A9_88    |
| CALAUTO_ENCODER_41L        | CALAUTO encoder 41L                       | A9_89    |
| CALAUTO_ENCODER_41R        | CALAUTO encoder 41R                       | A9_90    |
| CALAUTO_ENCODER_43L        | CALAUTO encoder 43L                       | A9_91    |
| CALAUTO_ENCODER_43R        | CALAUTO encoder 43R                       | A9_92    |
| CALAUTO_ENCODER_45L        | CALAUTO encoder 45L                       | A9_93    |
| CALAUTO_ENCODER_45R        | CALAUTO encoder 45R                       | A9_94    |
| CALAUTO_ENCODER_47L        | CALAUTO encoder 47L                       | A9_95    |
| CALAUTO_ENCODER_47R        | CALAUTO encoder 47R                       | A9_96    |
| H_FI_36BAR_PV              | 36 bar steam flow from boiler             | A9_97    |
| S9902A_PV                  | Press speed                               | A9_98    |
| S9902A_PV1                 | Press speed analog output                 | A9_99    |
| SETDRVSPEED                | Forming belt speed setpoint               | A9_100   |
| SETHTEMPCOOLINGAREA        | Cooling area temperature setpoint         | A9_101   |
| SETHTEMPHEATINGCIRCUIT1    | Heating circuit 1 temperature setpoint    | A9_102   |
| SETHTEMPHEATINGCIRCUIT2    | Heating circuit 2 temperature setpoint    | A9_103   |
| SETHTEMPHEATINGCIRCUIT3    | Heating circuit 3 temperature setpoint    | A9_104   |
| SETHTEMPHEATINGCIRCUIT4    | Heating circuit 4 temperature setpoint    | A9_105   |
| SETHTEMPHEATINGCIRCUIT5    | Heating circuit 5 temperature setpoint    | A9_106   |
| SETHTEMPHEATINGCIRCUIT6    | Heating circuit 6 temperature setpoint    | A9_107   |
| SETHTEMPHEATINGCIRCUIT7    | Heating circuit 7 temperature setpoint    | A9_108   |
| SETHTEMPPRESSUREPOTCOOL    | Pressure pot cooling temperature setpoint | A9_109   |
| SETPRDCOMPRESSIONCIRCUIT01 | Compression circuit 1 setpoint            | A9_110   |
| SETPRDCOMPRESSIONCIRCUIT02 | Compression circuit 2 setpoint            | A9_111   |
| SETPRDCOMPRESSIONCIRCUIT03 | Compression circuit 3 setpoint            | A9_112   |
| SETPRDCOMPRESSIONCIRCUIT04 | Compression circuit 4 setpoint            | A9_113   |
| SETPRDCOMPRESSIONCIRCUIT05 | Compression circuit 5 setpoint            | A9_114   |

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